

**EFFECT OF THERMAL RADIATION ON HYDROMAGNETIC COVECTIVE HEAT AND MASS
TRANSAFER FLOW OF A NANOFLUID IN A CYLINDRICAL ANNULUS
WITH CHEMICAL REACTION**

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ABSTRACT

In this Paper, we discuss the effect of thermo-diffusion on non-Darcy convective heat and mass transfer flow through a porous medium in a Co-axial cylindrical duct where the boundaries are maintained at temperature T_w and Concentration C_w . The behaviour of velocity, temperature and concentration is analyzed at different axial positions. The shear stress and the rate of heat and mass transfer have also been obtained for variations in the governing parameters.

Keywords: Nano Fluid, Cylindrical Annulus, MHD, Heat Sources, Thermal Radiation.

1. INTRODUCTION

The increasing cost of energy has led technologists to examine measures which could considerably reduce the usage of the natural source energy. Thermal insulations will continue to find increased use as engineers seek to reduce cost. Heat transfer in porous thermal insulation within vertical cylindrical annuli provide us insight into the mechanism of energy transport and enable engineers to use insulation more efficiently. In particular, design engineers require relationships between heat transfer geometry and boundary conditions which can be utilized in cost-benefit analysis to determine the amount of insulation that will yield the maximum investment.

Heat transfer inside horizontal/vertical annuli has many engineering applications particularly in heat exchangers, solar collectors, thermal storage systems and electronic components. Several applications use natural convection as the main heat transfer mechanism. Therefore, it is worth to understand the thermal behavior of such systems when natural convection is important. The first massive study on this flow geometry was accomplished by Kuhen and Goldstein [3, 4]. In their work, an experimental and numerical investigation was done when the ratio of gap width to inner cylinder diameter was 0.8 for water and air in the annulus. In their experimental study, it was found that transition from laminar to turbulent flow occurs at Rayleigh number 10^6 .

Present days, researchers are more concentrating on enhancement of heat transfer. The low thermal conductivity of conventional heat transfer fluids, such as water, is considered a primary limitation in enhancing the heat transfer performance. Maxwell's review [11] demonstrated the possibility of increasing the thermal conductivity of fluid-solid particles. Subsequently, the particles with micrometer or considerably millimeter measurements were utilized. Those particles caused several problems such as abrasion, clogging and pressure losses. During the past decade the technology of producing particles in nanometer dimensions was improved and a new kind of solid-liquid mixture that is called nanofluid was established by Choi [5]. The dispersion of a small amount of solid nanoparticle in conventional fluids such as water or Ethylene glycol changes their thermal conductivity remarkably. In general, in most recent research areas, heat transfer enhancement in forced convection is desirable [3, 4 and 16], but there is still a debate on the effect of nano-particles on heat transfer enhancement in natural convection applications. Natural convection of Al_2O_3 -water and CuO-water nanofluid inside a cylindrical enclosure heat from one side and cooled from the other side was studied by Putra *et al.*, [15]. They found that the natural convection heat transfer coefficient was lower than that of pure water.

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Wen and Ding [22] investigated the natural convection of TiO₂-water in a vessel composed of two discs. Their results showed that the natural convection decreases by increasing the volume fraction of nanoparticle. Jou and Tzeng [7] conducted a numerical study of natural convection heat transfer in rectangular enclosure filled with the stream function-vorticity formulation. They investigated the effects of Rayleigh number, the aspect ratio of the enclosure, and the volume fraction of the nanoparticle on the heat transfer inside the enclosures. Their results showed that the average heat transfer coefficient increased with increasing the volume fraction of the nanoparticle. Mokhtari Moghari *et al.* [12] studied two phase mixed convection Al₂O₃-water nanofluid flow in an annulus. Thermal conductivity variation on natural convection flow of water-alumina nanofluid in annulus is investigated by Parvin *et al.* [14]. Soleimani *et al.* [17] studied natural convection heat transfer in a nanofluid filled semi-annulus enclosure. Abu-Nada *et al.* [1] studied natural convection heat transfer enhancement in horizontal concentric annuli using nanofluid. Abu-Nada [2] investigated the effect of variable viscosity and thermal conductivity of Al₂O₃-water nanofluid on heat transfer enhancement in natural convection. Das *et al.* [6] have studied mixed convective magneto hydrodynamic flow in a vertical channel filled with nanofluids. Sreedevi *et al.* [18] has investigated mixed convective heat and mass transfer flow of nanofluids in concentric annulus with constant heat flux. NagaSasikala *et al.* [13] have investigated heat and mass transfer of a MHD flow of a nanofluid through a porous medium in an annular, circular region with outer cylinder maintained at constant heat flux. Sudarsana *et al.*, [20] have analyzed the Soret and Dufour effects on MHD convective flow of Al₂O₃-water and TiO₂-water nanofluids past a stretching sheet in porous media with heat generation with heat generation/absorption. Madhusudhana Reddy *et al.*, [10] have presented Numerical study of Convective Flow of CuO-water and Al₂O₃-water Nanofluids in cylindrical annulus. Srinivas *et al.*, [19] have discussed Particle spacing and chemical reaction effects on convective heat transfer through a nanofluid in cylindrical annulus. Recently Sulochana *et al.* [21] have discussed heat and mass transfer flow in cylindrical annulus in presence of heat sources.

In this paper we investigate the combined influence of magnetic field and thermal radiation on heat and mass transfer flow of nano fluid in cylindrical annulus. By employing FEM method the non linear governing equations have been solved. The effect of magnetic field (M), and Radiation (Rd) on all flow characteristics have been analyzed.

2. FORMULATION OF THE PROBLEM

We consider the free and forced convection flow in a vertical circular annulus through a porous medium whose walls are maintained at a constant heat flux and uniform concentration. The flow, temperature and concentration in the fluid are assumed to be fully developed. Both the fluid and porous region have constant physical properties and the flow is a mixed convection flow taking place under thermal and molecular buoyancies and uniform axial pressure gradient. The Boussinesque approximation is invoked so that the density variation is confined to the thermal and molecular buoyancy forces. The Brinkman-Forchheimer-Extended Darcy model which accounts for the inertia and boundary effects has been used for the momentum equation in the porous region. The momentum, energy and diffusion equations are coupled and non-linear. Also the flow is unidirectional along the axial direction of the cylindrical annulus. Making use of the above assumptions the governing equations are

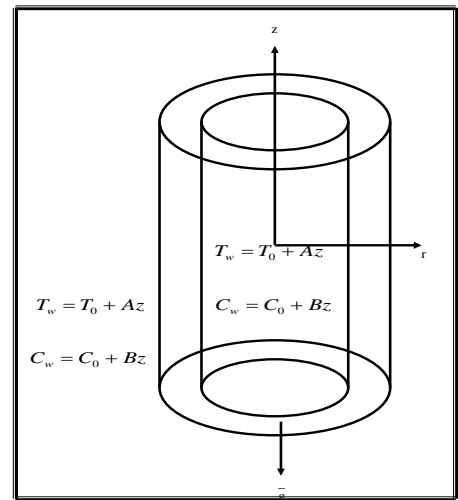


Fig.1 : CONFIGURATION OF THE PROBLEM

$$-\frac{\partial p}{\partial z} + \frac{\mu_{nf}}{\rho_{nf} \delta} \left(\frac{\partial^2 u}{\partial r^2} + \frac{1}{r} \frac{\partial u}{\partial r} \right) - \left(\frac{\mu_{nf}}{\rho_{nf} k} \right) u - \frac{\sigma_{nf} \mu_e^2 H_0^2}{\rho_{nf} r^2} - \frac{\delta F}{\rho_{nf} \sqrt{k}} u^2 + (\rho \beta)_{nf} (T - T_i) = 0 \quad (1)$$

$$(\rho C_p)_{nf} u \frac{\partial T}{\partial z} = k_{nf} \left(\frac{\partial^2 T}{\partial r^2} + \frac{1}{r} \frac{\partial T}{\partial r} \right) + Q_H (T - T_0) - \frac{1}{r} \frac{\partial (r q_R)}{\partial r} \quad (2)$$

$$u \frac{\partial C}{\partial z} = D_B \left(\frac{\partial^2 C}{\partial r^2} + \frac{1}{r} \frac{\partial C}{\partial r} \right) - k'_c C \quad (3)$$

where u is the axial velocity in the porous region, T , C are the temperature and concentration of the fluid, k is the permeability of porous medium, k_f is the thermal diffusivity, F is a function that depends on Reynolds number, the microstructure of the porous medium and D_B is the molecular diffusivity, β is the coefficient of the thermal expansion, Q_H is the heat source coefficient, Q_1 is the radiation absorption coefficient, C_p is the specific heat, ρ is density and g is gravity.

The relevant boundary conditions are

$$u = 0, \quad T=T_w, \quad C=C_w \text{ at } r = a \text{ \& \& } a+s \tag{4}$$

Following Tao(28a), we assume that the temperature and concentration of the both walls is $T_w = T_0 + Az$, $C_w = C_0 + Bz$ where A and B are the vertical temperature and concentration gradients which are positive for buoyancy –aided flow and negative for buoyancy –opposed flow, respectively, T_0 and C_0 are the upstream reference wall temperature and concentration, respectively. For the fully developed laminar flow in the presences of radial magnetic field, the velocity depend only on the radial coordinate and all the other physical variables except temperature, concentration and pressure are functions of r and z, z being the vertical co-ordinate. The temperature and concentration inside the fluid can be written as

$$T = T^\bullet(r) + Az, \quad C = C^\bullet(r) + Bz \tag{5}$$

The effective density of the nanofluid is given by

$$\rho_{nf} = (1-\phi)\rho_f + \phi\rho_s \tag{6}$$

Where ϕ is the solid volume fraction of nanoparticles

Thermal diffusivity of the nanofluid is

$$\alpha_{nf} = \frac{k_{nf}}{(\rho C_p)_{nf}} \tag{7}$$

Where the heat capacitance C_p of the nanofluid is obtained as

$$(\rho C_p)_{nf} = (1-\phi)(\rho C_p)_f + \phi(\rho C_p)_s \tag{8}$$

And the thermal conductivity of the nanofluid k_{nf} for spherical nanoparticles can be written as

$$\frac{k_{nf}}{k_f} = \frac{(k_s + 2k_f) - 2\phi(k_f - k_s)}{(k_s + 2k_f) + \phi(k_f - k_s)} \tag{9}$$

The thermal expansion coefficient of nanofluid can determine by

$$(\rho\beta)_{nf} = (1-\phi)(\rho\beta)_f + \phi(\rho\beta)_s \tag{10}$$

Also the effective dynamic viscosity of the nanofluid given by

$$\mu_{nf} = \frac{\mu_f}{(1-\phi)^{2.5}}, \tag{11}$$

$$\sigma_{nf} = \sigma_f \left(1 + \frac{3(\sigma-1)\phi}{\sigma+2-(\sigma-1)\phi}\right), \sigma = \frac{\sigma_s}{\sigma_f}$$

Where the subscripts nf, f and s represent the thermo physical properties of the nanofluid, base fluid and the nano solid particles respectively and ϕ is the solid volume fraction of the nanoparticles. The thermo physical properties of the nanofluid are given in Table 1.

Physical Properties	Fluid phase	CuO (Copper)	Al2O3 (Alumina)	TiO2 (Titanium dioxide)
Cp(j/kg K)	4179	385	765	686.2
$\rho(\text{kg m}^3)$	997.1	8933	3970	4250
k(W/m K)	0.613	400	40	8.9538
$\beta \times 10^{-5} \text{ 1/k}$	21	1.67	0.63	0.85

We now define the following non-dimensional variables

$$z^* = \frac{z}{a}, \quad r^* = \frac{r}{a}, \quad u^* = \left(\frac{a}{\nu}\right)u$$

$$p^* = \frac{pa\delta}{\rho\nu^2}, \theta^*(r^*) = \frac{T^\bullet - T_0}{P_1 Aa}, \quad C^*(r^*) = \frac{C^\bullet - C_0}{P_1 Ba}, \quad s^* = \frac{s}{a}, P_1 = \frac{dp}{dx}$$

Introducing these non-dimensional variables, the governing equations in the non-dimensional form are (on removing the stars)

$$\left(\frac{\partial^2 u}{\partial r^2} + \frac{1}{r} \frac{\partial u}{\partial r}\right) = 1 + \delta \left(D^{-1} + \frac{M^2}{r^2}\right) u + \delta^2 (D^{-1})^{1/2} \Delta u^2 - \delta G(\theta + NC) \quad (12)$$

$$\left(1 + \frac{4Rd}{3}\right) \left(\frac{\partial^2 \theta}{\partial r^2} + \frac{1}{r} \frac{\partial \theta}{\partial r}\right) = u + \frac{\alpha}{Pr} \theta \quad (13)$$

$$\left(\frac{\partial^2 C}{\partial r^2} + \frac{1}{r} \frac{\partial C}{\partial r}\right) - \gamma C = Sc u \quad (14)$$

where

$$\Delta = FD^{-1} \text{ (Inertia parameter or Forchhimer number), } G = \frac{g\beta(T_e - T_i)a^3}{\nu^2} \text{ (Grashof number)}$$

$$D^{-1} = \frac{a^2}{k} \text{ (Inverse Darcy parameter), } M^2 = \frac{\sigma\mu_e^2 H_0^2}{a\nu} \text{ (Hartmann number)}$$

$$Pr = \frac{\mu C_p}{k_f} \text{ (Prandtl number), } Sc = \frac{\nu}{D_B} \text{ (Schmidt number), } \alpha = \frac{Qa^2}{C_p k_f} \text{ (Heat Source parameter)}$$

$$\gamma = \frac{k_c^1 a^2}{D_B} \text{ (Chemical Reaction parameter), } Rd = \frac{4\sigma^* T_e^3}{\beta r k_f} \text{ (Radiation parameter)}$$

The corresponding non-dimensional conditions are

$$u = 0, \quad \theta = 0, \quad C = 0 \quad \text{at } r=1 \text{ and } 1+s \quad (15)$$

3. FINITE ELEMENT ANALYSIS

The finite element analysis with quadratic polynomial approximation functions is carried out along the radial distance across the circular duct. The behavior of the velocity, temperature and concentration profiles has been discussed computationally for different variations in governing parameters. The Galerkin method has been adopted in the variational formulation in each element to obtain the global coupled matrices for the velocity, temperature and concentration in course of the finite element analysis.

Choose an arbitrary element e_k and let u^k, θ^k and C^k be the values of u, θ and C in the element e_k

We define the error residuals as

$$E_p^k = \frac{d}{dr} \left(r \frac{du^k}{dr} \right) + \delta G(\theta^k) - \delta \left(D^{-1} + \frac{M^2}{r^2} \right) ru^k - \delta^2 \Delta r (u^k)^2 \quad (6.10)$$

$$E_\theta^k = \frac{1}{Pr} \frac{d}{dr} \left(r \frac{d\theta^k}{dr} \right) - ru^k + \frac{\alpha}{Pr} r\theta \quad (16)$$

$$E_c^k = \frac{d}{dr} \left(r \frac{dC^k}{dr} \right) - rScu^k - \gamma C^k \quad (17)$$

where u^k, θ^k & C^k are values of u, θ & C in the arbitrary element e_k . These are expressed as linear combinations in terms of respective local nodal values.

$$u^k = u_1^k \psi_1^k + u_2^k \psi_2^k + u_3^k \psi_3^k, \quad \theta^k = \theta_1^k \psi_1^k + \theta_2^k \psi_2^k + \theta_3^k \psi_3^k, \quad C^k = C_1^k \psi_1^k + C_2^k \psi_2^k + C_3^k \psi_3^k$$

where $\psi_1^k, \psi_2^k, \dots$ etc are Lagrange's quadratic polynomials.

Galerkin's method is used to convert the partial differential Eqs. (16) – (17) into matrix form of equations which results into 3x3 local stiffness matrices. All these local matrices are assembled in a global matrix by substituting the global nodal values of order I and using inter element continuity and equilibrium conditions.

The shear stress (τ), Nusselt number (rate of heat transfer), Sherwood number (rate of mass transfer) are evaluated by using the following formulas

$$\tau = \left(\frac{du}{dr} \right)_{r=1,1+s}, \quad Nu = - \left(\frac{d\theta}{dr} \right)_{r=1,1+s}, \quad Sh = - \left(\frac{dC}{dr} \right)_{r=1,1+s}$$

Comparison: In the absence of magnetic field ($M=0$), Thermal radiation ($Rd=0$) the results are in good agreement with Sulochana *et al.* [21].

Parameter	Sulochana et al [21]		Present Results		Sulochana et al [21]		Present Results		
	CuO-water		CuO-water		Al ₂ O ₃		Al ₂ O ₃		
	$\tau(1)$	$\tau(2)$	$\tau(1)$	$\tau(2)$	Nu(1)	Nu(2)	Nu(1)	Nu(2)	
ϕ	0.05	-0.344709	0.295543	-0.344712	0.295541	-0.375427	0.309548	-0.375426	0.309549
	0.1	-0.322286	0.234133	-0.322288	0.234129	-0.356835	0.243367	-0.356834	0.243369
	0.3	-0.298190	0.199080	-0.298192	0.199075	-0.305607	0.155813	-0.305601	0.155816
	0.5	-0.166095	0.166046	-0.166089	0.166042	-0.204787	0.125445	-0.204782	0.125449
Δ	2	-0.344709	0.295543	-0.344702	0.295539	-0.375427	0.309548	-0.375424	0.309551
	4	-0.835576	0.757665	-0.835569	0.757659	-0.904463	0.866134	-0.904459	0.866136
	6	-1.793485	1.213450	-1.793481	1.213452	-1.855349	1.234368	-1.855342	1.234366
	10	-2.329867	2.148234	-2.329862	2.148236	-2.454894	2.357145	-2.454896	2.357142

6. RESULTS AND DISCUSSION

The equations governing the flow, heat and mass transfer have been solved by employing Galerkin finite element analysis with quadratic approximation polynomials. We have chosen here $\Delta=6.2$ while M , D^{-1} , α , Rd , ϕ, Δ , are varied over a range, which are listed in the Figure legends.

Fig.2 represents the effect of magnetic parameter M on the nanofluid velocity profile. It is observed from the figure that the velocity distribution increases with increasing magnetic parameter $M \leq 4$ and for higher $M \geq 6$, we notice a reduction in the velocity. This enhancement can be attributed to the fact that the magnetic field provides a resistive type of force known as the Lorentz force. This force tends to lessen the motion of the fluid for higher values of $M \geq 6$ as a consequence the velocity reduces. We also find that the nano-fluid velocity in the case of CuO – water nanofluid is relatively lesser than that of Al₂O₃-water nanofluid. This phenomenon has good agreement with the physical realities. Fig.9 represents the effect of magnetic parameter M on the nanofluid temperature profile. It is observed from the figure that the temperature distribution increases with increasing values of M and it exhibits a decreasing tendency for higher $M \geq 6$, as a result of increase in the thickness of the thermal boundary layer owing to the Lorentz force developed by the magnetic field. We also find that the nano-fluid temperature in the case of CuO – water nanofluid is relatively greater than that of Al₂O₃-water nanofluid. This phenomenon has good agreement with the physical realities Fig.16 represents the effect of M on the nanofluid concentration profile. It is observed from the figure that the concentration distribution increases with increasing values of M as a result of enhancement of the thickness of the solutal boundary layer. We also find that the nanofluid concentration in the case of CuO-water nanofluid is relatively lesser than that of Al₂O₃-water nanofluid. This phenomenon has good agreement with the physical realities.

Fig.3 represents the effect of inverse Darcy parameter D^{-1} on the nanofluid velocity profile. It is observed from the figure that the velocity distribution decreases with increasing the inverse Darcy parameter D^{-1} . This is due to the fact that increase in the obstruction of the fluid motion with increase in the inverse Darcy parameter. We also find that the nano-fluid velocity in the case of CuO – water nanofluid is relatively lesser than that of Al₂O₃-water nanofluid. This phenomenon has good agreement with the physical realities. Fig.10 represents the effect of inverse Darcy parameter D^{-1} on the nanofluid temperature profile. It is observed from the figure that the temperature distribution increases with increasing values of D^{-1} as a result of increase in the thickness of the thermal boundary layer owing to the Darcy drag developed by the porous medium.. We also find that the nano-fluid temperature in the case of CuO – water nanofluid is relatively greater than that of Al₂O₃-water nanofluid. This phenomenon has good agreement with the physical realities Fig.17 represents the effect of inverse Darcy parameter D^{-1} on the nanofluid concentration profile. It is observed from the figure that the concentration distribution increases with increasing values of D^{-1} as a result of increasing the thickness of the solutal boundary layer owing to the Darcy drag developed by the porous medium. We also find that the nano-fluid concentration in the case of CuO-water nanofluid is relatively smaller than that of Al₂O₃-water nanofluid. This phenomenon has good agreement with the physical realities.

The velocity, temperature enhances while the concentration reduces with increase in the strength of the heat generating source and in the case of heat absorption source, the velocity reduces, the temperature and concentration enhances in the flow region. The skin friction enhances with increase in $\alpha > 0$ and reduces with $\alpha < 0$ on both the cylinders (Figs.4, 5, 11, 12).

The variation of velocity with Radiation parameter (Rd) is exhibited in Fig.6. It is found that velocity shows an enhancement with increasing the values of Rd in the flow region. This is due to the fact that the thickness of the boundary layer increases with values of Rd in both types of nanofluids. Fig.13 shows the variation of temperature with Rd. It is found that an increase in Rd enhances the temperature in the thermal boundary layer. Thus lesser the radiative heat flux larger the temperature in the flow region. We also note that the temperature in Al₂O₃-water nanofluid is relatively smaller than that of CuO-water nanofluid.

Fig.7 display the effect of nanoparticle volume fraction ϕ on the nanofluid velocity. It is found that as the nanoparticle volume fraction decreases the nanofluid velocity in both types of nanofluids. These figures illustrate this agreement with the physical behaviour. When the volume of the nanoparticle reduces the thermal conductivity and hence reduces the momentum boundary layer thickness. We also notice that the nanofluid velocity in the case of Al₂O₃ – water nanofluid is relatively greater than that of CuO-water nanofluid. Fig.14 shows that the variation of temperature with ϕ . It can be seen from the profiles that an increase in the nanoparticle volume fraction reduces the temperature in the boundary layer. This is due to the fact that the thickness of the thermal boundary layer decreases with increase in ϕ . Also we find that the temperature in Al₂O₃-water is relatively lesser than that of CuO-water fluid. Fig.19 shows the variation of concentration with nanoparticle volume fraction ϕ . We notice a reduction in the concentration with increasing ϕ . This may be attributed to the fact that an enhancement in ϕ results in decreasing the thickness of the solutal boundary layer. The concentration in CuO-water nanofluid is smaller than those values of C in Al₂O₃-water nanofluid.

The variation of velocity with Δ is exhibited in Fig.8. It is found that velocity shows an enhancement with increasing the values of Δ in the flow region. This is due to the fact that the thickness of the boundary layer increases with values of Δ in both types of nanofluids. Fig.17 shows the variation of temperature with Δ . It is found that an increase in Δ enhances the temperature in the thermal boundary layer. Thus lesser the thermal diffusivity larger the temperature in the flow region.. We also note that the temperature in Al₂O₃-water nanofluid is relatively smaller than that of CuO-water nanofluid.

The table 3 displays the behaviour of local skin friction (τ) at the inner and outer cylinders $r=1&2$. The variation of τ with magnetic parameter M & D-1 shows that higher the Lorentz force /Lesser the permeability of the porous medium larger the skin friction at $r=1&2$ in both types of nanofluids. The rate of heat transfer on $r=1&2$ with increase in the strength of the heat generating/absorbing source. The Sherwood number reduces on $r=1$ with increase in the strength of the heat generating/absorption source while a reversed effect is noticed on the $r=2$. The rate of heat transfer reduces on the inner cylinder and enhances on the outer cylinder with increase in $\alpha>0$ and in the case of $\alpha<0$, a reversed effect is noticed in the behaviour of Nu on the both the cylinders.

The variation of τ with radiation parameter Rd shows that higher the radiative heat flux smaller the magnitude of the skin friction on the both walls. With respect to Δ , we find that lesser the thermal diffusivity, smaller the skin friction at both the cylinders in both types of nanofluid. From the tabular values of the skin friction with different parametric variations we find that the magnitude of skin friction in CuO-water nanofluid is relatively lesser than those values in Al₂O₃-water nanofluid. Also the magnitude of the skin friction at the inner cylinder is relatively larger than those on the outer cylinder for all variations.

The local Nusselt number (Nu) at the inner and outer cylinders $r=1&2$ is shown in table 3 for different parametric variations. The rate of heat transfer in the CuO-water nanofluid is relatively lesser than those values in Al₂O₃-water nanofluid. With respect to variation of Nu with magnetic parameter M we find that higher the Lorentz force/lesser the permeability of the porous medium larger the rate of heat transfer at $r=1&2$ in both types of nanofluids. We observed that the Nusselt number in CuO-water nanofluid is relatively smaller than those values in Al₂O₃-water nanofluid. The rate of heat transfer with radiation parameter Rd shows that higher the radiative heat flux larger the Nusselt number at both the cylinders. An increase in the Nanoparticle volume fraction ϕ reduces Nu at $r=1&2$ in CuO-water and Al₂O₃-water nanofluids. The rate of heat transfer in the CuO-water nanofluid is relatively lesser than those values in Al₂O₃-water nanofluid. The variation of Nu with Prandtl number Pr shows that |Nu| increases with increase in Pr. and |Nu| in CuO-water nanofluid are lesser than those values in Al₂O₃-water nanofluid.

The table 4 represents the variation of mass transfer Sh at $r=1&2$ with different values of M, D-1, Rd, ϕ and Δ . An increase M and D-1 enhances |Sh| at $r=1&2$ in both types of nanofluids. Also we find that |Sh| in CuO-water nanofluid is relatively lesser than those values in Al₂O₃-water nanofluid. With respect to Schmidt number Sc we find that an increase in Sc enhances |Sh| at $r=1&2$ in both types of nanofluids. |Sh| at $r=1&2$ in CuO-water nanofluid are relatively lesser than those of Al₂O₃-water nanofluid. The variation of Sh with Chemical reaction parameter γ shows that |Sh| at $r=1&2$ reduces in CuO-water nanofluid and enhances it in Al₂O₃-water nanofluid in degenerating chemical reaction case, while in generating chemical reaction case |Sh| enhances in CuO-water nanofluid at $r=2$ and reduces at $r=1$ In the case of Al₂O₃-water nano fluid, the Sherwood number reduces on both the cylinders. In both the degenerating and generating chemical reaction case we find that the vales of |Sh| at cylinders in CuO-water nanofluid are relatively

smaller than those values in Al_2O_3 -water nanofluid. With reference to Rd we find that the rate of mass transfer reduces with increasing values of Rd on both the cylinders in both types of nanofluids. The variation of Sh with Nano particle volume fraction ϕ shows that the rate of mass transfer reduces at $r=1$ & 2 with increase in ϕ in CuO -water and Al_2O_3 -water nanofluids.

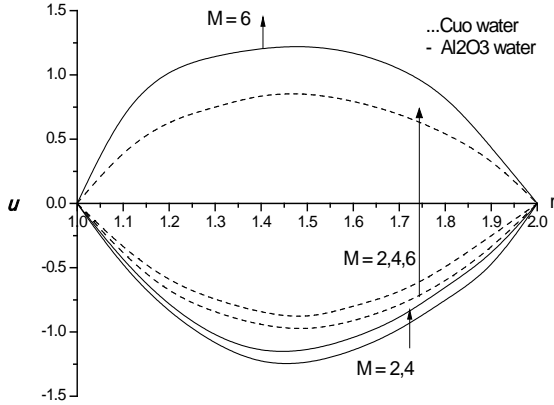


Fig. 2 : Variation of u with M
 $D^{-1}=0.2, \alpha=2, Rd=0.5, \phi=0.1, \Delta=2$

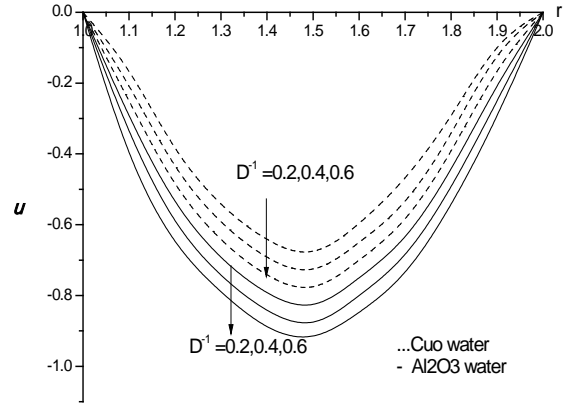


Fig. 3 : Variation of u with D^{-1}
 $M=2, \alpha=2, Rd=0.5, \phi=0.1, \Delta=2$

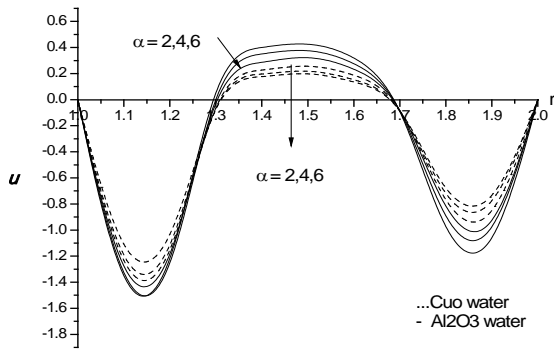


Fig. 4 : Variation of u with $\alpha > 0$
 $M=2, D^{-1}=0.2, Rd=0.5, \phi=0.1, \Delta=2$

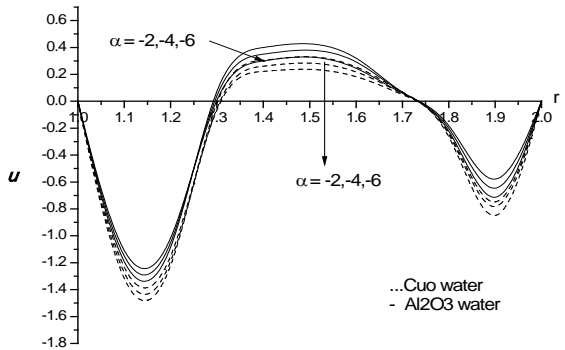


Fig. 5 : Variation of u with $\alpha < 0$
 $M=2, D^{-1}=0.2, Rd=0.5, \phi=0.1, \Delta=2$

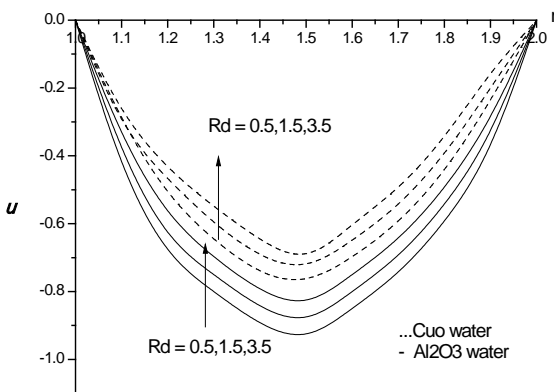


Fig. 6 : Variation of u with Rd
 $M=2, D^{-1}=0.2, \alpha=2, \phi=0.1, \Delta=2$

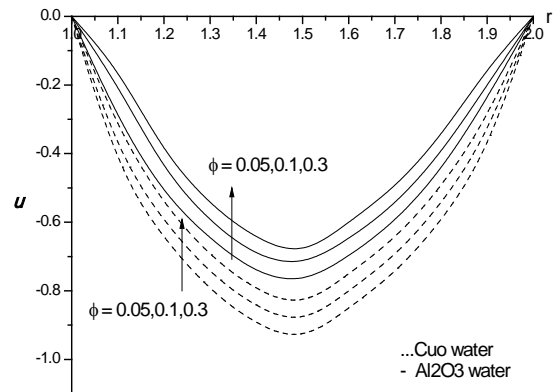


Fig. 7 : Variation of u with ϕ
 $M=2, D^{-1}=0.2, \alpha=2, Rd=0.1, \Delta=2$

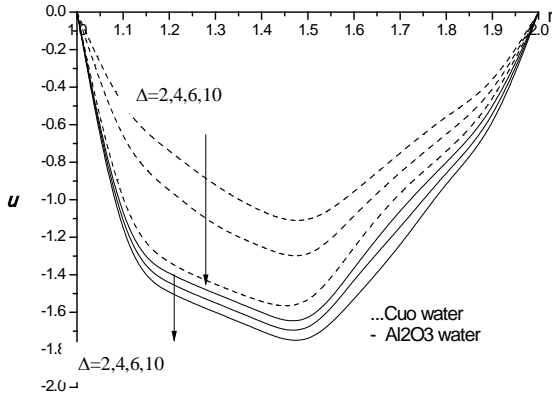


Fig. 8 : Variation of u with Δ
 $M=2, D^{-1}=0.2, \alpha=2, Rd=0.1, \phi=0.5$

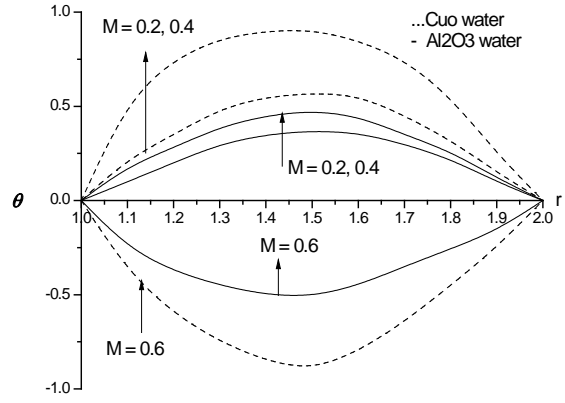


Fig. 9 : Variation of θ with M
 $D^{-1}=0.2, \alpha=2, Rd=0.1, \phi=0.1, \Delta=2$

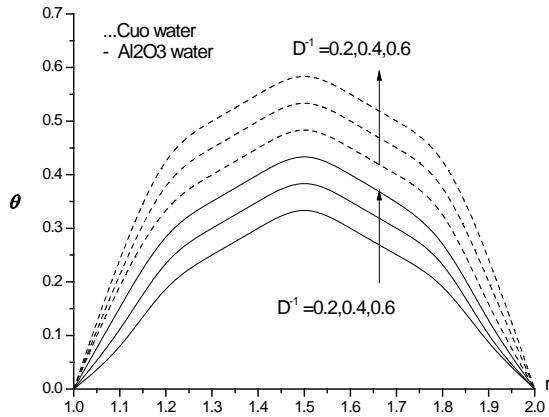


Fig. 10 : Variation of θ with D^{-1}
 $M=2, \alpha=2, Rd=0.5, \phi=0.1, \Delta=2$

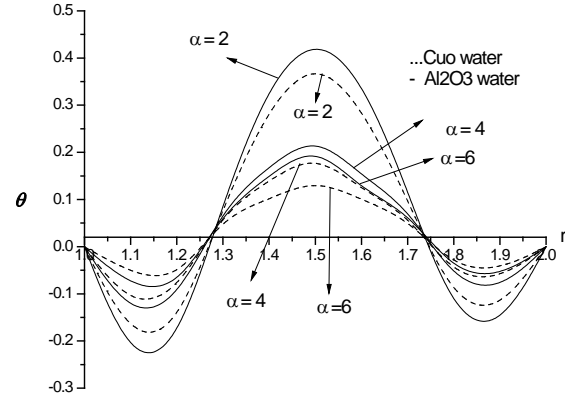


Fig. 11 : Variation of θ with $\alpha > 0$
 $M=2, D^{-1}=0.2, Rd=0.5, \phi=0.1, \Delta=2$

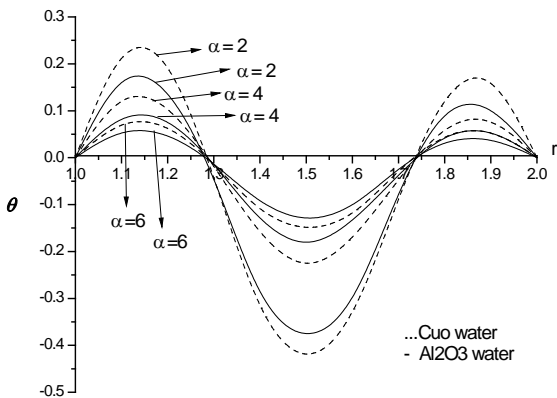


Fig. 12 : Variation of θ with $\alpha < 0$
 $M=2, D^{-1}=0.2, Rd=0.5, \phi=0.1, \Delta=2$

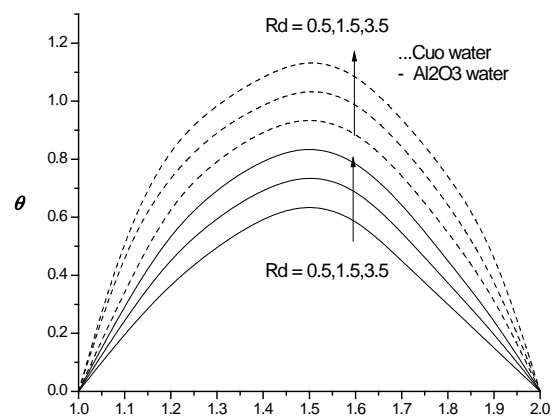


Fig. 13 : Variation of θ with Rd
 $M=2, D^{-1}=0.2, \alpha=2, \phi=0.1, \Delta=2$

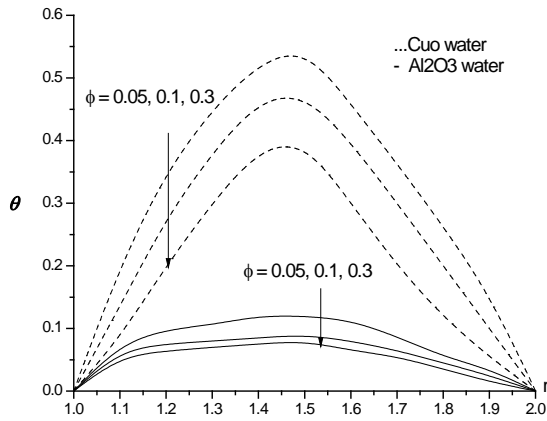


Fig. 14 : Variation of θ with ϕ
 $M=2, D^{-1}=0.2, \alpha=2, Rd=0.5, \Delta=2$

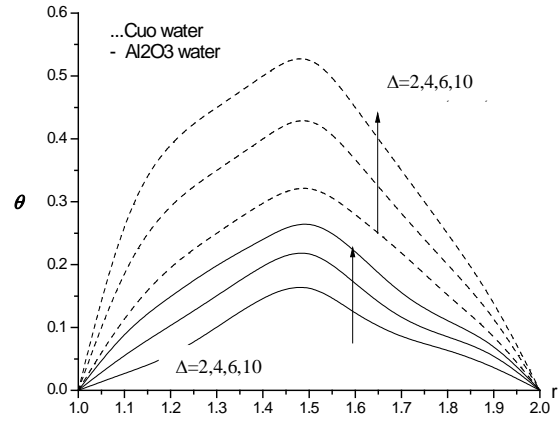


Fig. 15 : Variation of θ with Δ
 $M=2, D^{-1}=0.2, \alpha=2, Rd=0.5, \phi=0.1$

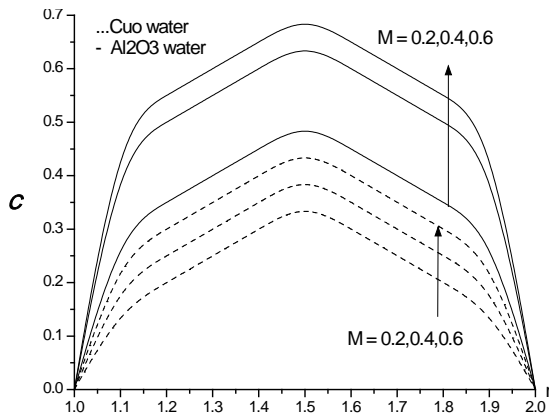


Fig. 16 : Variation of C with M
 $D^{-1}=0.2, Rd=0.5, \phi=0.1, \Delta=2$

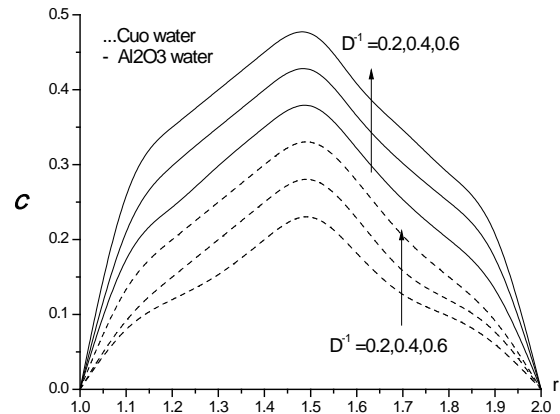


Fig. 17 : Variation of C with D^{-1}
 $M=2, Rd=0.5, \phi=0.1, \Delta=2$

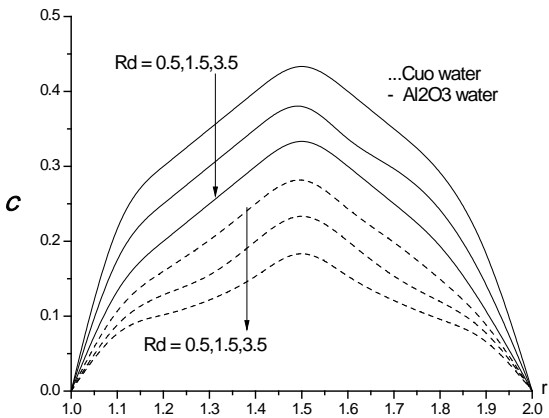


Fig. 18: Variation of C with Rd
 $M=2, D^{-1}=0.2, \phi=0.1, \Delta=2$

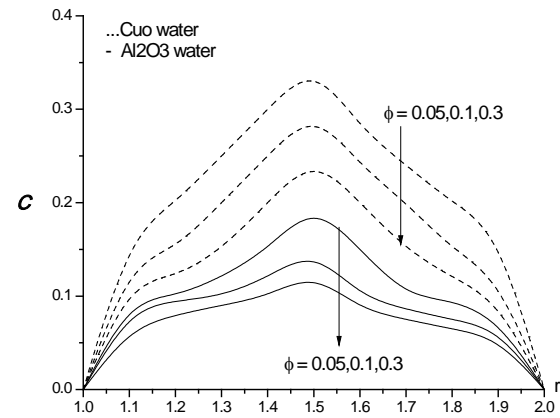


Fig. 19 : Variation of C with ϕ
 $M=2, D^{-1}=0.2, Rd=0.5, \Delta=2$

Table--2: Skin Friction (τ) at the boundaries $r = 1$ and 2 .

Parameter		CuO-water		Al ₂ O ₃ -water	
		$\tau(1)$	$\tau(2)$	$\tau(1)$	$\tau(2)$
M	0.5	-0.346	0.271	-0.347827	0.272488
	1.5	-0.397	0.299	-0.399628	0.300678
	3.0	-0.413	0.368	-0.530861	0.370653
D⁻¹	0.2	-0.34	0.271	0.34827	0.272481
	0.4	-0.376	0.293	-0.378611	0.294481
	0.6	-0.413	0.319	-0.416042	0.321161
α	2	-0.23717	0.16968	-0.238486	0.170687
	4	-0.23577	0.16861	-0.236415	0.169107
	-2	-0.23166	0.16547	-0.230429	0.164534
	-4	-0.23301	0.16651	-0.232387	0.166031
Rd	0.5	-0.346	0.271	-0.34827	0.272484
	2.5	-0.344	0.270	-0.34679	0.272378
	3.5	-0.343	0.269	-0.347529	0.27227
	5.0	-0.342	0.267	-0.347475	0.272232
ϕ	0.05	-0.346	0.271	-0.347828	0.272484
	0.1	-0.268	0.133	-0.168935	0.133677
	0.3	-0.101	0.080	-0.0731107	0.058131
	0.5	-0.058	0.046	-0.0558487	0.044451
Δ	2	-0.346	0.271	-0.347824	0.272484
	4	-0.835	0.655	-0.844163	0.661346
	6	-1.796	1.410	-1.83489	1.43768
	10	-3.329	2.618	-3.46394	2.71458

Table – 3: Nusselt Number (Nu) at the boundaries $r = 1$ and 2 .

Parameter		CuO-water		Al ₂ O ₃ -water	
		Nu (1)	Nu (2)	Nu (1)	Nu (2)
M	0.5	0.21577	-0.1690	0.21665	-0.169721
	1.5	0.24774	-0.1864	0.248915	-0.187283
	3.0	0.32856	-0.2295	0.330656	-0.230868
D⁻¹	0.2	0.2157	-0.1690	0.21665	-0.169721
	0.4	0.23476	-0.1826	0.235825	-0.183425
	0.6	0.25784	-0.1991	0.259139	-0.200041
α	2	-0.4166	0.2977	-0.418512	0.299534
	4	-0.2066	0.1477	-0.207154	0.148175
	-2	0.4042	-0.2885	0.402134	-0.287137
	-4	0.2036	-0.1454	0.203057	-0.145076
Rd	0.5	0.21577	-0.1690	0.21665	-0.169721
	1.5	0.41708	-0.3269	0.420377	-0.329331
	3.5	0.56867	-0.4459	0.626608	-0.490914
	5.0	0.61932	-0.4856	0.700219	-0.548591
ϕ	0.05	0.21577	-0.1690	0.21665	-0.169721
	0.1	0.10506	-0.0831	0.105224	-0.832153
	0.3	0.06348	-0.0503	0.045538	-0.362082
	0.5	0.03618	-0.0287	0.034786	-0.276868
Δ	2	0.21577	-0.1690	0.21665	-0.169721
	4	1.26448	-0.9914	1.29542	-1.01488
	6	5.9144	-4.6426	6.12841	-4.80175
	10	6.1074	-5.63095	7.21889	-6.171528

Table – 4: Sherwood Number (Sh) at the boundaries $r = 1$ and 2 .

Parameter		CuO-water		Al ₂ O ₃ -water	
		Sh (1)	Sh (2)	Sh (1)	Sh (2)
M	0.5	0.219086	-0.158652	0.220067	0.15935
	1.5	0.250915	-0.179936	0.252234	0.180842
	3.0	0.330908	-0.233166	0.333139	0.234712
D⁻¹	0.2	0.219086	-0.158652	0.220067	-0.15935
	0.4	0.240309	-0.173749	0.241491	-0.174589
	0.6	0.266106	-0.192088	0.267558	-0.193119
α	2	0.747845	0.748776	-0.736189	0.739688
	4	0.760395	0.758563	-0.754633	0.754069
	-2	-0.787312	0.787312	-0.808339	0.796016
	-4	-0.785074	0.777829	-0.790703	0.782227
Rd	0.5	0.219086	-0.158652	0.220067	-0.15935
	1.5	0.218977	-0.157928	0.219964	-0.15927
	3.5	0.217305	-0.157384	0.219863	-0.159202
	5.0	0.217045	-0.157202	0.219823	-0.159176
Sc	0.24	0.040446	-0.0292895	0.0406278	-0.0294195
	0.66	0.111228	-0.0805462	0.112133	-0.0811948
	1.3	0.219086	-0.158652	0.220067	-0.15935
γ	0.5	0.219086	-0.158652	0.220067	-0.15935
	1.5	0.0415453	-0.0300361	0.246593	-0.178267
	-0.5	0.0334789	-0.0242815	0.198714	-0.144114
	-1.5	0.0305212	-0.0221693	0.181158	-0.131572
φ	0.05	0.219086	-0.158652	0.220067	-0.15935
	0.1	0.106332	-0.077171	0.106509	-0.0772964
	0.3	0.0641656	-0.0466089	0.045996	-0.0334261
	0.5	0.0365028	-0.0265309	0.0351252	-0.0255302
Δ	2	0.219086	-0.158652	0.220067	-0.15935
	4	0.528328	-0.382636	0.534066	-0.386715
	6	1.13396	-0.821456	1.16069	-0.840484
	10	2.09737	-1.519998	2.19075	-1.586456

7. CONCLUSIONS

The coupled equations governing the flow, heat and mass transfer have been solved by using Galerkin finite method with quadratic approximation functions. The velocity, temperature and concentration have been analysed for different parametric variations. The important conclusions of the analysis are

- Higher the Lorentz force smaller the velocity and temperature, larger the concentration. The skin friction, the rate of heat and mass transfer reduces on the cylinders with increase in M .
- The velocity, temperature enhances while the concentration reduces with increase in the strength of the heat generating source and in the case of heat absorption source, the velocity reduces, the temperature and concentration enhances in the flow region. The skin friction enhances with increase in $\alpha > 0$ and reduces with $\alpha < 0$ on both the cylinders. The rate of heat transfer on $r=1$ & 2 with increase in the strength of the heat generating/absorbing source. The Sherwood number reduces on $r=1$ with increase in the strength of the heat generating/absorption source while a reversed effect is noticed on the $r=2$. The rate of heat transfer reduces on the inner cylinder and enhances on the outer cylinder with increase in $\alpha > 0$ and in the case of $\alpha < 0$, a reversed effect is noticed in the behaviour of Nu on the both the cylinders.
- An increasing Rd increases velocity and temperature.
- An increase in nano particle concentration reduces a velocity, temperature and concentration.
- With reference to the chemical reaction parameter γ , we find that the velocity, temperature and concentration enhance in the flow region in the degenerating chemical reaction case while in the generating chemical reaction case, they reduces in the flow region. The skin friction, Nusselt number and Sherwood number enhance in the degenerating chemical reaction case while in generating case a reversed effect is noticed on the cylinders.

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