

**EFFECT OF UNSTEADY FLOW  
IN A ROTATING PARALLEL PLATE CHANNEL WITH A POROUS BED**

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**ABSTRACT**

*In this Paper we make an initial value investigation of the flow of an incompressible viscous fluid in rotating channel bounded above by a rigid plane and below by the porous bed abutting the impermeable boundary plane. The flow in the non-porous region is governed Navaier-Stokes equations while the Brinkman model is used in the porous bed. The perturbations in the flow are created by the constant pressure gradient along in the plate in addition to non-torsional oscillations of the lower plate. Initial value problem has been solved making use of transform techniques and exact solution of velocity in the clean fluid and the porous region are evaluated. The velocity field consists of steady state, quasi steady state and the transient components. The time required for the decay of the transient term is discussed and the ultimate quasi steady state solution is analyzed with focus on its physical nature. The stresses on the boundary planes have also been evaluated. The behavior of the velocity and the stress with reference to variations in the governing parameters namely  $E$ , the Ekman number,  $D$ , the Darcy parameter and  $h$ , the non dimensional thickness of bed has been computationally discussed.*

**Keywords:** *unsteady flow, Porous bed, Brinkman model.*

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**1. INTRODUCTION**

The channel flow problems where the flow is maintained by torsional or non-torsional oscillations of one or both the boundaries, throw some light in finding out the growth and development of boundary layers associated with flows occurring in geothermal phenomena. Claire Jacob [4] has studied the transient effects considering the small amplitude torsional oscillations of disks. This problem has been extended to the hydro-magnetic case by Murthy [7], who discussed torsional oscillations of the disks maintained at different temperatures. Debnath [5] has considered an unsteady hydrodynamic and hydromagnetic boundary flow in a rotating viscous fluid due to oscillations of plates including the effects of uniform pressure gradients and uniform suction. The structure of the velocity field and the associated Stokes, Ekman and Rayleigh boundary layers on the plates are determined for the resonant and non-resonant cases. Rao, D.R.V., Krishna, D.V. & Debanath, L. [10] have made an initial value investigation of the combined free and forced convection effects in an unsteady hydromagnetic viscous incompressible rotating fluid between two disks under a uniform transverse magnetic field. This analysis has been extended to porous boundaries by Sarojamma and Krishna [13] and later by Siva Prasad [14,17,18,19] to include the Hall current effects.

All fluid phenomena on earth involve rotation to a greater or lesser extent. Because of the basic rotation of the earth most of the large scale motions of the atmosphere and the sea fall under the category in which rotation is an absolutely essential factor. The atmosphere and the oceans are compressible fluids, but in many cases the essential physical features of atmospheric and oceanic flows are not dependent on this fact and fairly satisfactory theories can be based on mathematical models assuming an incompressible fluid. The atmosphere and the oceans are located on earth which is a spheroid (almost a sphere) and their scale of motion is relatively small compared to the earth radius.

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The fact that the geophysical fluids are really thin spherical shells is felt in such models in two different ways: a) there are purely geometrical effects associated with any planar map of the sphere and b) the angular velocity vector of the rotating sphere makes different angles with the vertical at different latitudes. The geometrical effects do not seem to be of qualitative importance except when the motions are of a scale comparable to the radius, but the effects of the rotating sphere in some respects create qualitative differences already on an intermediate scale.

Because of the fact that the geophysical flows normally have a horizontal scale large compared to the vertical scale, the velocity vectors are nearly horizontal and in such cases where a small range of latitude is involved, the vertical component may be regarded as constant. A satisfactory model is obtained by considering a plane horizontal layer of fluid rotating about a vertical axis with angular velocity equal to the vertical component  $\Omega \sin \lambda$  where  $\lambda$  is the latitude of the earth's angular velocity. This is commonly called the "f-plane model" because the parameter measuring the rotation which occurs in the equations, for same basic equations as in the f-plane model, except that  $f$  is no longer taken as constant, but its variation with latitude is included. A simplified version of this is called the " $\beta$ -Plane Model" ( $\beta$  is the measure of the rate of change of  $f$  with latitude); It does not consider the geometrical effects of the spherical surface, but takes partial account of the variation with the mathematical complexities. There is another interesting aspect of the problem of rotating, viscous fluid. Here viscous boundary layers are formed on the solid bodies and there exists a strong interaction between the boundary layers and the outer flow.

A detailed account of the motion of rotating fluids enclosed within a body or vice versa was given by Greenspan (6). An example relating to such interaction for the flow of a fluid under a constant pressure gradient between two rotating parallel plates was given by Vidyandhi (16). This rotating viscous flow equations yield a layer flow known as the Ekman boundary layer, named after the Swedish oceanographer V. Walfried Ekman who discovered this phenomenon. Attempts to observe the structure of the Ekman layer in the surface layers of the sea have been successful. Ekman layers are easy to produce and observe them in the laboratory. Such boundary layers, or similar ones, are required to connect principally geostrophic flow in the interior of the fluid to horizontal boundaries where conditions like a prescribed horizontal stress, or no-slip on a solid bottom, are given. In similar way, other kinds of viscous boundary layer have been studied so as to connect geostrophic flows to vertical boundaries (for example a vertical well along which the depth varies) on which boundary conditions in consistent with geostrophic flow are given.

There is a considerable interest in past and recent years in the study of flow past a naturally permeable bed, with appropriate boundary conditions at a naturally permeable boundary. The usual conditions are, the normal flux is continuous and the tangential velocity is zero. The former is completely satisfactory but the latter is clearly only an approximation. As an alternative to this no-slip boundary conditions Beavers & Joseph (1) have postulated, for the first time, the slip boundary conditions which they verified it experimentally. The existence of the slip at the porous bed, due to the transfer of momentum from the free flow to Darcy flow which sets up the drag, is connected with presence of a very thin boundary layer of stream wise moving fluid just beneath the nominal surface of the permeable material. The fluid in this layer is pulled along by the flow in the channel.

Although the experiments were performed by Beavers & Joseph (1) to test the validity of the proposed slip boundary conditions, owing to inadequate apparatus and instruments, the accuracy of experimental results was not sufficient to permit conclusive evaluation of the proposed analytical model but the existence of a slip velocity was confirmed qualitatively. Later experiments by Beavers, Sparrow & Magnuson (2), Taylor (15) & Rajasekhara (8) have further confirmed the existence of the slip at the nominal surface. Saffman (12) gave a rigorous theoretical proof for the existence of the slip at the nominal surface postulated Beavers & Joseph (1). Rajasekhara, Ramaiah & Rudraiah (9) have investigated a steady laminar flow of forced convection through a channel having on porous bounding wall. They have taken into account the velocity slip at the surface of the porous medium and the contribution of heat due to viscous dissipation.

Although the slip at the nominal surface was established based on the existence of a thin boundary layer just beneath the nominal surface, attention was not focused on the analytical determination of the boundary layer thickness. Later Rudraiah, Rajasekhara & Ramaiah (9), Channabasappa & Rangann (3) have determined analytically this boundary layer thickness. Rudraiah & Veerabhadrarai (11) extended this analysis to include the buoyancy force.

Rajasekhara (8) has performed the experiments to study the laminar flow characteristics in a composite channel considering Poiseuille flow, Couette flow and free surface flow. The aim of his experimental study was to determine the values of the slip parameter lower than that of Beavers & Joseph (1). Such lower values are of importance in the design of porous bearings. Auxillar experiments were also conducted to measure the values of  $k$ , the permeability of the porous medium. His experimental results were found to be in fair agreement with the analytical model which contains slip velocity at the permeable surface, except the mass flow rate which shows a slight deviation between experimental and theoretical data. Rudraiah & Veerabhadrarai (11) have pointed out that this deviation may be due to the neglect of buoyancy force narrow down the deviation of the theoretical results from the experimental data for a particular value of the buoyancy parameter.

## 2. FORMULATION OF THE PROBLEM

We consider the unsteady flow of an incompressible viscous fluid in a rotating parallel plate channel bounded below by a porous matrix abutting an impermeable wall. The clean fluid region above the porous matrix is bounded by an impermeable wall and is governed by the Navier – Stokes equations. The flow in the porous region is governed by equations based on Brinkman model. In the undisturbed state both the plates and the fluid rotate with the same angular velocity  $\Omega$ . At  $t > 0$ , the fluid is driven by a constant pressure gradient parallel to the plate and in addition the lower plate performs non – torsional oscillations in its own plane.

We choose a Cartesian Co – ordinate system  $O(x, y, z)$  such that the plates are at  $z = 0$  and  $z = H$  and the  $z$  – axis coincides with the axis of rotation of the plates. The entire region is divided into two zones, Zone – I (clean fluid region) and Zone – II (porous region), the interface of two regions is assumed to be  $z = h$ . The unsteady hydrodynamic boundary layer equations of motion with respect to a rotating frame moving with angular velocity  $\Omega$  are as follows.

The equations governing the clean fluid region (Zone – I i.e., Navier – Stokes equations) are

$$\frac{\partial u}{\partial t} + 2\Omega v = -\frac{1}{\rho} \frac{\partial p}{\partial x} + \nu \frac{\partial^2 u}{\partial z^2} \quad (1)$$

$$\frac{\partial v}{\partial t} - 2\Omega u = -\frac{1}{\rho} \frac{\partial p}{\partial y} + \nu \frac{\partial^2 v}{\partial z^2} \quad (2)$$

Where  $u, v$  are components of the velocity along  $O(x, y)$  directions and  $-\frac{\partial p}{\partial x}$  and  $-\frac{\partial p}{\partial y}$  are components of the imposed pressure gradient along  $O(x, y)$  directions respectively. Here  $\rho$  is the density and  $\nu$  is the coefficient of Kinematic viscosity of the fluid.

The equations governing the flow in the porous region (Brinkman model) i.e., Zone – II are

$$\frac{\partial u_p}{\partial t} + 2\Omega v_p = -\frac{1}{\rho} \frac{\partial p}{\partial x} + \nu_{eff} \frac{\partial^2 u_p}{\partial z^2} - \frac{\nu}{k} u_p \quad (3)$$

$$\frac{\partial v_p}{\partial t} - 2\Omega u_p = -\frac{1}{\rho} \frac{\partial p}{\partial y} + \nu_{eff} \frac{\partial^2 v_p}{\partial z^2} - \frac{\nu}{k} v_p \quad (4)$$

Where  $u_p, v_p$  are the components of the velocity along in the porous region along  $O(x, y)$  directions respectively. Here  $\nu_{eff}$  is the coefficient of Kinematic Viscosity in the porous medium and  $k$  is permeability of the porous medium.

In view of the equations of continuity of the fluid flow in either zones,  $u, v$  and  $u_p, v_p$  are functions of  $z, t$  alone, since the boundary planes extended to infinity along  $x, y$  directions. In the absence of any extraneous forces in  $z$  – direction, the pressure is a function of  $x, y$ . For practical purposes we may assume  $\nu = \nu_{eff}$ .

The boundary conditions relevant to Zone – I are

$$u = 0, v = 0 \text{ on } z = H, \quad u = u_p \text{ at } z = h.$$

The boundary conditions relevant to Zone – II are

$$u_p = a \exp(i \omega t) + b \exp(-i \omega t) \text{ on } z = 0 \\ v_p = 0 \text{ on } z = 0.$$

At the interface  $z = h$ ,

$$\frac{\partial u}{\partial z} = \frac{\partial u_p}{\partial z}, \quad \frac{\partial v}{\partial z} = \frac{\partial v_p}{\partial z}.$$

The initial conditions are

$$u = 0, v = 0 \text{ at } t = 0; \\ u_p = 0, v_p = 0 \text{ at } t = 0.$$

Now, we define  $q = u + i v, q_p = u_p + i v_p$  and  $\xi = x - i y$

Combining (2.1), (2.2), (2.3), and (2.4), we obtain

$$\frac{\partial q}{\partial t} - 2i\Omega q - \nu \frac{\partial^2 q}{\partial z^2} = -\frac{1}{\rho} \frac{\partial p}{\partial \xi} \quad (5)$$

$$\frac{\partial q_p}{\partial t} - 2i\Omega q_p - \nu \frac{\partial^2 q_p}{\partial z^2} + \frac{\nu}{k} q_p = -\frac{1}{\rho} \frac{\partial p}{\partial \xi} \quad (6)$$

We now define the non-dimensional variables

$$h' = \frac{h}{H}, \quad z' = \frac{z}{H}, \quad \xi' = \frac{\xi}{H}, \quad q' = \frac{qH'}{\nu},$$

$$q_p' = \frac{q_p H'}{\nu}, \quad t' = \frac{t\nu}{H'^2}, \quad w' = \frac{wH'^2}{\nu}, \quad p' = \frac{pH'^3}{\nu^2}.$$

Substituting these in (2.5) and (2.6), the equations governing the flow in non-dimensional form (on dropping the dashes) are

$$\frac{\partial q}{\partial t} - 2iE^{-1}q - \frac{\partial^2 q}{\partial z^2} = p \quad (7)$$

$$\frac{\partial q_p}{\partial t} - 2iE^{-1}q_p - \frac{\partial^2 q_p}{\partial z^2} + D^{-1}q_p = p \quad (8)$$

Where  $E = \frac{\nu}{\Omega h^2}$  is the Ekman number and  $D = \frac{k}{h^2}$  is the Darcy parameter.

The boundary conditions in the non-dimensional form are

$$q(z,0) = 0 \text{ on } z = 1 \quad (9)$$

$$q_p = a \exp(i\omega t) + b \exp(-i\omega t) \text{ on } z = 0 \quad (10)$$

Where a and b are constants.

The initial conditions are

$$q(z, 0) = 0; q_p(z, 0) = 0.$$

The interfacial conditions are

$$(q)_{z=h} = (q_p)_{z=h} \quad (11)$$

$$\left( \frac{\partial q}{\partial z} \right)_{z=h} = \left( \frac{\partial q_p}{\partial z} \right)_{z=h} \quad (12)$$

Taking Laplace Transforms, the governing equations (2.7) and (2.8) reduces to

$$[D^2 + (2iE^{-1} - s)]\bar{q} = -\frac{P}{s}$$

$$[D^2 - (s - 2iE^{-1} + D^{-1})]\bar{q}_p = -\frac{P}{s}, \quad \text{where } D = \frac{d}{dz}$$

The solutions of (7) and (8) satisfying the boundary conditions are

$$\bar{q} = -\frac{\lambda_2 \lambda_3}{\lambda_4} \sinh \lambda_1 (1-z) - \frac{P}{s \lambda_2 \lambda_4} \cosh \lambda_2 h \sinh \lambda_1 (1-z) + \frac{P}{s \lambda_1^2 \lambda_4} \lambda_2 \cosh \lambda_2 h \sinh \lambda_1 (1-z)$$

$$- \frac{P}{s \lambda_1^2 \lambda_4} \frac{\lambda_2 \cosh \lambda_2 h \cosh \lambda_1 h \sinh \lambda_1 (1-z)}{\cosh \lambda_1} + \frac{P}{s \lambda_1 \lambda_4} \frac{\sinh \lambda_1 h \sinh \lambda_2 h \sinh \lambda_1 (1-z)}{\cosh \lambda_1} - \frac{P}{s \lambda_1^2} \frac{\cosh \lambda_1 z}{\cosh \lambda_1} + \frac{P}{s \lambda_1^2}$$

$$\bar{q}_p = \lambda_3 \cosh \lambda_2 z - \frac{\lambda_2 \lambda_3}{\lambda_4} \frac{\sinh \lambda_2 z \sinh \lambda_1 (1-h)}{\sinh \lambda_2 h} - \frac{P}{s \lambda_2 \lambda_4} \cosh \lambda_2 h \frac{\sinh \lambda_2 z}{\sinh \lambda_2 h} \sinh \lambda_1 (1-h)$$

$$+ \frac{P}{s \lambda_1^2 \lambda_4} \frac{\lambda_2 \cosh \lambda_2 h \sinh \lambda_1 (1-h) \sinh \lambda_2 z}{\sinh \lambda_2 h} - \frac{P \lambda_2 \cosh \lambda_1 h \cosh \lambda_2 h}{s \lambda_1^2 \lambda_4 \cosh \lambda_1} \sinh \lambda_1 (1-h) \frac{\sinh \lambda_2 z}{\sinh \lambda_2 h}$$

$$\begin{aligned}
 & + \frac{p}{s\lambda_1\lambda_4} \frac{\sinh\lambda_1 h \sin h\lambda_1(1-h)}{\cosh\lambda_1} \sinh\lambda_2 z - \frac{p}{s\lambda_1^2} \frac{\cosh\lambda_1 h \sinh\lambda_2 z}{\cosh\lambda_1 \sinh\lambda_2 h} \\
 & + \frac{p}{s\lambda_1^2} \frac{\sinh\lambda_2 z}{\sinh\lambda_2 h} - \frac{\lambda_3 \cosh\lambda_2 h \sinh\lambda_2 z}{\sinh\lambda_2 h} - \frac{p}{s\lambda_2^2} \frac{\sinh\lambda_2 z}{\sinh\lambda_2 h} + \frac{p}{s\lambda_2^2}
 \end{aligned}$$

Here  $\lambda_1 = \sqrt{s-2iE^{-1}}$ ,  $\lambda_2 = \sqrt{s-2iE^{-1}+D^{-1}}$ ,  
 $\lambda_3 = \frac{a}{s-iw} + \frac{b}{s+iw} - \frac{p}{s\lambda_2^2}$ ,  
 $\lambda_4 = -[\lambda_1 \sinh\lambda_2 h \cosh\lambda_1(1-h) + \lambda_2 \cosh\lambda_2 h \sinh\lambda_1(1-h)]$

From the above expressions, we note that,  $\bar{q}$  &  $\bar{q}_p$  have singularities at  
 $s = 0$ ,  $s = \pm iw$ ,  $S = 2i E^{-1}$ ,  $s = 2i E^{-1} - D^{-1}$ ,  $s = (2i E^{-1} - (2n+1)2 \frac{\pi^2}{4})$ .

Evaluating the Laplace inversion, we obtain

$$\begin{aligned}
 q = u + i v = & -\frac{p}{2iE^{-1}} + \frac{p}{2iE^{-1}} \frac{\cosh a_5 z}{\cosh a_5} - \frac{p \sinh a_5 h \sinh a_4 h \sinh a_5(1-z)}{a_5 b_2 \cosh a_5} \\
 & - \frac{p a_4 \cosh a_4 h \cosh a_5 h \sinh a_5(1-z)}{2b_2 i E^{-1} \cosh a_5} + \frac{p a_4 \sinh a_5(1-z)}{b_2 a_7} + \frac{p \cosh a_4 h \sinh a_5(1-z)}{b_2 a_4} \\
 & + \frac{p a_4 \cosh a_4 h \sinh a_5(1-z)}{2ib_2 E^{-1}} + \frac{a a_o \sinh a_1(1-z) e^{i\omega t}}{b_o} + \frac{b a_2 \sinh a_3(1-z) e^{-i\omega t}}{b_1} \\
 & + \sum_{n=0}^{\infty} \frac{4 p \cos(2n+1) \frac{\pi}{2} z}{a_o i \pi^2 (2n+1)^2 \sin(2n+1) \frac{\pi}{2}} e^{a_6 t} \\
 q_p = u_p + i v_p = & -\frac{p}{a_7} - \frac{p}{2iE^{-1}} \frac{\sinh a_4 z}{\sinh a_4 h} + \frac{p}{a_7} \frac{\sinh a_4 z}{\sinh a_4 h} + \frac{p}{a_7} \cosh a_4 z - \frac{p}{a_7} \frac{\cosh a_4 h \sinh a_4 z}{\sinh a_4 h} \\
 & + \frac{p \cosh a_5 h \sinh a_4 z}{2iE^{-1} \cosh a_5 \sinh a_4 h} + \frac{p a_4 \sinh a_5(1-h) \sinh a_4 z}{a_7 b_2 \sinh a_4 h} \\
 & - \frac{p \cosh a_4 h \sinh a_4 z \sinh a_5(1-h)}{a_4 b_2 \sinh a_4 h} - \frac{p \sinh a_5 h \sinh a_5(1-h) \sinh a_4 z}{a_5 b_2 \cosh a_5} \\
 & - \frac{p a_4 \cosh a_4 h \sinh a_5(1-h) \sinh a_4 z}{2ib_2 E^{-1} \sinh a_4 h \cosh a_5} - (a \cosh a_7 z) e^{i\omega t} + (b \cosh a_2 z) e^{-i\omega t} \\
 & + \frac{a a_o \sinh a_1(1-h) \sinh a_o z}{b_o \sinh a_o h} e^{i\omega t} + \frac{b a_2 \sinh a_3(1-h) \sinh a_2 z}{b_1 \sinh a_2 h} e^{-i\omega t} \\
 & - \frac{a \cosh a_o h \sinh a_o z e^{i\omega t}}{\sinh a_o h} - \frac{b \cosh a_2 h \sinh a_2 z}{\sinh a_2 h} e^{-i\omega t} + \sum_{n=1}^{\infty} \frac{4 p \cos\left(\frac{(2n+1)\pi}{2}\right) h}{i a_o \pi^2 (2n+1)^2} \frac{\sinh a_8 z}{\sinh a_8 h} e^{a_6 t} \\
 & - \frac{a D^{-\frac{1}{2}} \sinh D^{-\frac{1}{2}} z e^{2iE^{-1}t}}{b_3 \sinh D^{-\frac{1}{2}} h} \left( a_{11} - \frac{a_9 t^{\frac{1}{2}}}{6\sqrt{\pi} b_3 a_{11}} - \frac{t^{\frac{1}{2}}}{\sqrt{\pi} (a_{11})^2} + \frac{t^{\frac{3}{2}}}{2\sqrt{\pi}} \left\{ \frac{a_{10}}{120 b_3 a_{11}} - (a_{11})^3 - \frac{a_9}{6 b_3 (a_{11})^2} \right\} \right)
 \end{aligned}$$

$$\begin{aligned}
 & - \frac{bD^{-\frac{1}{2}} \sinh D^{-\frac{1}{2}} z e^{2iE^{-1}t}}{b_3 \sinh D^{-\frac{1}{2}} h} \left( a_{12} - \frac{a_9 t^{\frac{1}{2}}}{6\sqrt{\pi} b_3 a_{12}} - \frac{t^{\frac{1}{2}}}{\sqrt{\pi} (a_{12})^2} + \frac{t^{\frac{3}{2}}}{2\sqrt{\pi}} \left\{ \frac{a_{10} a_{12}}{120 b_3} - (a_{12})^3 - \frac{a_9}{6 b_3 (a_{11})^2} \right\} \right) \\
 & + \frac{p \sinh D^{-\frac{1}{2}} z e^{2iE^{-1}t}}{2iE^{-1} D^{-\frac{1}{2}} \sinh D^{-\frac{1}{2}} h b_3} \times \left( 1 - \frac{a_9 t^{\frac{1}{2}}}{6\sqrt{\pi} b_3} - \frac{t^{\frac{1}{2}}}{\sqrt{\pi} 2iE^{-1}} + \frac{t^{\frac{3}{2}}}{8\sqrt{\pi} E^{-2}} - \frac{a_9 t^{\frac{3}{2}}}{48 i b_3 E^{-1} \sqrt{\pi}} + \frac{t^{\frac{3}{2}}}{2\sqrt{\pi}} \frac{a_{10}}{120 b_3} \right) \\
 & (1 - \cosh D^{-\frac{1}{2}} h)
 \end{aligned}$$

### 3. SHEAR STRESS

The non-dimensional Shear Stress  $\tau_x$  and  $\tau_y$  are obtained at the lower and upper plates from  $q$  and  $\bar{q}$  are given by

$$\begin{aligned}
 (\tau_x + i\tau_y)_{z=0} &= \left( \frac{\partial q_p}{\partial z} \right)_{z=0} & (\tau_x + i\tau_y)_{z=1} &= \left( \frac{\partial \bar{q}}{\partial z} \right)_{z=1} \\
 \left( \frac{\partial q}{\partial z} \right)_{z=1} &= - \frac{pa_4 a_5}{b_2 a_7} - \frac{pa_4 a_5 \cosh a_4 h \cosh a_5 h}{2iE^{-1} \cosh a_5} + \frac{p \sinh a_5 h \sinh a_4 h}{b_2 \cosh a_5} - \frac{pa_5 \cosh a_4 h}{a_4 b_2} \\
 & - \frac{pa_4 a_5 \cosh a_4 h}{2iE^{-1} b_2} + \frac{pa_5 \sinh a_5}{2iE^{-1} \cosh a_5} - \frac{aa_o a_1 e^{i\omega t}}{b_1} - \frac{ba_2 a_3 e^{-i\omega t}}{b_1} - \sum_{n=1}^{\infty} \frac{2pe^{a_6 t}}{i(2n+1)\pi a_6} \\
 \left( \frac{\partial q_p}{\partial z} \right)_{z=0} &= - \frac{pa_4 \cosh a_4 h}{a_7 \sinh a_4 h} - \frac{pa_4 \cosh a_4 h \sinh a_5 (1-h)}{a_4 b_2 \sinh a_4 h} + \frac{pa_4^2 \cosh a_4 h \sinh a_5 (1-h)}{2b_2 iE^{-1} \sinh a_5 h} \\
 & - \frac{pa_4^2 \cosh a_4 h \sinh a_5 (1-h)}{2b_2 iE^{-1} \sinh a_4 h \cosh a_5} - \frac{pa_4 \sinh a_5 h \sinh a_5 (1-h)}{a_5 b_2 \cosh a_5} + \frac{pa_4 \cosh a_5 h}{2iE^{-1} \cosh a_5 \sinh a_4 h} \\
 & - \frac{pa_4}{2iE^{-1} \sinh a_4 h} + \frac{pa_4 \cosh a_4 h}{a_7 \sinh a_4 h} - \frac{aa_o \cosh a_4 h e^{i\omega t}}{\sinh a_4 h} - \frac{ba_2 \cosh a_2 h e^{-i\omega t}}{\sinh a_2 h} \\
 & + \frac{aa_o^2 \sinh a_1 (1-h) e^{i\omega t}}{b_o \sinh a_1 h} + \frac{ba_2^2 \sinh a_3 (1-h) e^{-i\omega t}}{b_1 \sinh a_2 h} + \sum_{n=1}^{\infty} \frac{4pa_8}{i(2n+1)^2 \pi^2 a_6 \sinh a_8 h} e^{a_6 t} \\
 & - \frac{a D^{-1} e^{2iE^{-1}t}}{b_3 \sinh D^{-\frac{1}{2}} h} \left[ a_{11} - \frac{1}{\sqrt{\pi}} \frac{a_9 a_{11}}{6b_3} t^{\frac{1}{2}} - \frac{1}{\sqrt{\pi}} (a_{11})^2 t^{\frac{1}{2}} (a_{11})^3 + \frac{t^{\frac{3}{2}}}{2\sqrt{\pi}} \left\{ \frac{a_{10} a_{11}}{120 b_3} - \frac{(a_{11})^2 a_9}{6 b_3} \right\} \right] \\
 & - \frac{bD^{-1} e^{2iE^{-1}t}}{b_3 \sinh D^{-\frac{1}{2}} h} \left[ a_{12} - \frac{t^{\frac{1}{2}}}{\sqrt{\pi}} \frac{a_9 a_{12}}{6b_3} - \frac{(a_{12})^2 t^{\frac{1}{2}}}{\sqrt{\pi}} + \frac{a_{12} a_{10} t^{\frac{3}{2}}}{240 b_3 \sqrt{\pi}} - \frac{1}{\sqrt{\pi}} \frac{t^{\frac{1}{2}}}{6b_3} \frac{a_9 a_{12}}{6b_3} - \frac{(a_{12})^3 t^{\frac{3}{2}}}{2\sqrt{\pi}} - \frac{a_9 (a_{12})^2 t^{\frac{3}{2}}}{12 b_3 \sqrt{\pi}} \right] \\
 & + \frac{pD^{-1} e^{2iE^{-1}t}}{2iE^{-1} \sinh D^{-\frac{1}{2}} h b_3} \times \left( 1 - \frac{1}{\sqrt{\pi}} \frac{a_9 t^{\frac{1}{2}}}{6b_3} - \frac{1}{\sqrt{\pi}} \frac{t^{\frac{1}{2}}}{2iE^{-1}} + \frac{1}{8\sqrt{\pi}} \frac{t^{\frac{3}{2}}}{E^{-2}} - \frac{1}{48 iE^{-1} \sqrt{\pi}} \frac{a_9}{b_3} + \frac{t^{\frac{3}{2}}}{240 \sqrt{\pi}} \frac{a_{10}}{b_3} \right) \\
 & (1 - \cosh D^{-\frac{1}{2}} h)
 \end{aligned}$$

The Stress  $\tau_x$  and  $\tau_y$  on the upper and lower plate are evaluated for variations in E,  $D^{-1}$ , h and are tabulated in tables 1 to 8. From tables 1 - 4, we notice  $\tau_x$  and  $\tau_y$  increase in magnitude for increase in E while reduces with increase in  $D^{-1}$  for fixed values of the other parameters. The growth of stresses for increase in E is much rapid in comparison to its depreciation with increase in  $D^{-1}$ . In contrast, on the lower plate (tables 5 - 8)  $\tau_x$  reduces to with increase in E while  $\tau_y$  enhances with E although they do not depend on the depth of the porous lining and remains invariant with h, the thickness of bed reference to  $D^{-1}$ . We observe that the lower permeability lesser the magnitude of both  $\tau_x$  and  $\tau_y$  for fixed values of the other parameters.

**Table – 1:** Stress ( $\tau_x$ ) on upper plate  $D^{-1} = 10000$  ( $p=1$ ,  $\omega = \frac{\pi}{2}$ ,  $a=b=1$ ,  $t=1$ )

E	0.01	0.02	0.03	0.04	0.05
h = 0.2	-0.050037	-0.0700797	-0.0850257	-0.0993085	-0.114289
h = 0.3	-0.0500047	-0.069533	-0.0858304	-0.102975	-0.121221
h = 0.4	-0.0497412	-0.0696516	-0.08945	-0.110868	-0.132519
h = 0.5	-0.0492016	-0.0723844	-0.0980127	-0.123349	-0.145822
h = 0.6	-0.0495376	-0.0807752	-0.111086	-0.134781	-0.151822

**Table – 2:** Stress ( $\tau_x$ ) on upper plate  $E = 0.02$  ( $p=1$ ,  $\omega = \frac{\pi}{2}$ ,  $a=b=1$ ,  $t=1$ )

$D^{-1}$	$10^3$	$5 \times 10^3$	$10 \times 10^3$
h = 0.2	-0.0702025	-0.0701034	-0.0700797
h = 0.3	-0.0696253	-0.0695483	-0.069533
h = 0.4	-0.0694169	-0.0696013	-0.0696516
h = 0.5	-0.0712494	-0.0721602	-0.0723844
h = 0.6	-0.0781685	-0.0802787	-0.0807752

**Table – 3:** Stress ( $\tau_y$ ) on upper plate  $D^{-1} = 10000$  ( $p=1$ ,  $\omega = \frac{\pi}{2}$ ,  $a=b=1$ ,  $t=1$ )

E	0.01	0.02	0.03	0.04	0.05
h = 0.2	-0.0499783	-0.0705584	-0.0882533	-0.104938	-0.120104
h = 0.3	-0.0498835	-0.0713024	-0.0906362	-0.10781	-0.121903
h = 0.4	-0.0498181	-0.0731886	-0.0934921	-0.108951	-0.11918
h = 0.5	-0.0503205	-0.0760316	-0.0940286	-0.103402	-0.106243
h = 0.6	-0.0523256	-0.0765914	-0.0850556	-0.0839489	-0.0788995

**Table – 4:** Stress ( $\tau_y$ ) on upper plate  $E = 0.02$  ( $p=1$ ,  $\omega = \frac{\pi}{2}$ ,  $a=b=1$ ,  $t=1$ )

$D^{-1}$	$10^3$	$5 \times 10^3$	$10 \times 10^3$
h = 0.2	-0.0704542	-0.0705421	-0.0705584
h = 0.3	-0.0710112	-0.071246	-0.0713024
h = 0.4	-0.072614	-0.0730804	-0.0731886
h = 0.5	-0.0754396	-0.0759281	-0.0760316
h = 0.6	-0.0772434	-0.0767445	-0.0765914

**Table – 5:** Stress ( $\tau_x$ ) on lower plate  $D^{-1} = 10000$  ( $p=1$ ,  $\omega = \frac{\pi}{2}$ ,  $a=b=1$ ,  $t=1$ )

E	0.01	0.02	0.03	0.04	0.05
h = 0.4	0.0101555	0.0100782	0.0100522	0.0100392	0.0100313

**Table – 6:** Stress ( $\tau_x$ ) on lower plate  $E = 0.02$  ( $p=1$ ,  $\omega = \frac{\pi}{2}$ ,  $a=b=1$ ,  $t=1$ )

$D^{-1}$	$10^3$	$5 \times 10^3$	$10 \times 10^3$
h = 0.2	0.0275916	0.014359	0.0100782
h = 0.3	0.033644	0.0143621	0.0100782
h = 0.4	0.0339565	0.0143621	0.0100782
h = 0.5	0.0339725	0.0143621	0.0100782
h = 0.6	0.0339733	0.0143621	0.0100782

**Table – 7:** Stress ( $\tau_y$ ) on lower plate  $D^{-1} = 10000$  ( $p=1$ ,  $\omega = \frac{\pi}{2}$ ,  $a=b=1$ ,  $t=1$ )

E	0.01	0.02	0.03	0.04	0.05
h = 0.4	-0.0156056	-0.0156573	-0.0156743	-0.0156827	-0.0156878

**Table – 8:** Stress ( $\tau_y$ ) on lower plate  $E = 0.02$  ( $p=1$ ,  $\omega = \frac{\pi}{2}$ ,  $a=b=1$ ,  $t=1$ )

$D^{-1}$	$10^3$	$5 \times 10^3$	$10 \times 10^3$
$h = 0.2$	-0.0356716	-0.0220561	-0.0156573
$h = 0.3$	-0.0474457	-0.0220697	-0.0156574
$h = 0.4$	-0.0478992	-0.0220697	-0.0156574
$h = 0.5$	-0.0479161	-0.0220697	-0.0156574
$h = 0.6$	-0.0479166	-0.0220697	-0.0156574

We shall now discuss the velocity in both the clean fluid and the porous regions in the parallel plate channel subjected to a uniform rotation. The resultant flow is due to the inter play between the coriolis force and Darcy force. The velocity field in the clean fluid and porous region consists of the steady state terms, quasi steady oscillatory terms due to the non – torsional oscillations of the boundary plate and the unsteady time – decaying terms. In the clean fluid region

the transient terms decay in Dimensionless time of order  $\frac{4}{\pi^2}$  and in the porous region the infinite series of terms

decay in time or order  $[D^{-2} + (w - 2E^{-1})^2]^{-\frac{1}{4}}$ , the remaining finite time-dependent terms arising out of branch

points singularities in the transformed solution decay in time of order  $t^{-\frac{1}{2}}$ . When these transient decay term, the quasi steady state solution for the velocity component in both clean fluid region as well as porous region are given by

$$q = u + i v = -\frac{p}{2iE^{-1}} + \frac{p}{2iE^{-1}} \frac{\cosh a_5 z}{\cosh a_5} - \frac{p \sinh a_5 h \sinh a_4 h \sinh a_5 (1-z)}{a_5 b_2 \cosh a_5} \\ - \frac{p a_4 \cosh a_4 h \cosh a_5 h \sinh a_5 (1-z)}{2b_2 i E^{-1} \cosh a_5} + \frac{p a_4 \sinh a_5 (1-z)}{b_2 a_7} \\ + \frac{p \cosh a_4 h \sinh a_5 (1-z)}{b_2 a_4} + \frac{p a_4 \cosh a_4 h \sinh a_5 (1-z)}{2i b_2 E^{-1}} \\ + \frac{a a_0 \sinh a_1 (1-z) e^{i\omega t}}{b_0} + \frac{b a_2 \sinh a_3 (1-z) e^{-i\omega t}}{b_1}$$

$$q_p = u_p + i v_p = -\frac{p}{a_7} - \frac{p}{2iE^{-1}} \frac{\sinh a_4 z}{\sinh a_4 h} + \frac{p}{a_7} \frac{\sinh a_4 z}{\sinh a_4 h} + \frac{p}{a_7} \cosh a_4 z - \frac{p}{a_7} \frac{\cosh a_4 h \sinh a_4 z}{\sinh a_4 h} \\ + \frac{p \cosh a_5 h \sinh a_4 z}{2iE^{-1} \cosh a_5 \sinh a_4 h} + \frac{p a_4 \sinh a_5 (1-h) \sinh a_4 z}{a_7 b_2 \sinh a_4 h} \\ - \frac{p \cosh a_4 h \sinh a_4 z \sinh a_5 (1-h)}{a_4 b_2 \sinh a_4 h} - \frac{p \sinh a_5 h \sinh a_5 (1-h) \sinh a_4 z}{a_5 b_2 \cosh a_5} \\ - \frac{p a_4 \cosh a_4 h \sinh a_5 (1-h) \sinh a_4 z}{2i b_2 E^{-1} \sinh a_4 h \cosh a_5} (a \cosh a_0 z) e^{i\omega t} + (b \cosh a_2 z) e^{-i\omega t} \\ + \frac{a a_0 \sinh a_1 (1-h) \sinh a_0 z}{b_0 \sinh a_0 h} e^{i\omega t} + \frac{b a_2 \sinh a_3 (1-h) \sinh a_2 z}{b_1 \sinh a_2 h} e^{-i\omega t} \\ - \frac{a \cosh a_0 h \sinh a_0 z e^{i\omega t}}{\sinh a_0 h} - \frac{b \cosh a_2 h \sinh a_2 z}{\sinh a_2 h} e^{-i\omega t} \\ - \frac{a D^{-\frac{1}{2}} \sinh D^{-\frac{1}{2}} z e^{2iE^{-1}t}}{b_3 \sinh D^{-\frac{1}{2}} h} \left( a_{11} - \frac{a_9 t^{\frac{1}{2}}}{6\sqrt{\pi} b_3 a_{11}} - \frac{t^{\frac{1}{2}}}{\sqrt{\pi} (a_{11})^2} + \frac{t^{\frac{3}{2}}}{2\sqrt{\pi}} \left\{ \frac{a_{10}}{120 b_3 a_{11}} - (a_{11})^3 - \frac{a_9}{6 b_3 (a_{11})^2} \right\} \right) \\ - \frac{b D^{-\frac{1}{2}} \sinh D^{-\frac{1}{2}} z e^{2iE^{-1}t}}{b_3 \sinh D^{-\frac{1}{2}} h} \left( a_{12} - \frac{a_9 t^{\frac{1}{2}}}{6\sqrt{\pi} b_3 a_{12}} - \frac{t^{\frac{1}{2}}}{\sqrt{\pi} (a_{12})^2} + \frac{t^{\frac{3}{2}}}{2\sqrt{\pi}} \left\{ \frac{a_{10} a_{12}}{120 b_3} - (a_{12})^3 - \frac{a_9}{6 b_3 (a_{11})^2} \right\} \right)$$



$$+ \frac{p \sinh D^{\frac{1}{2}} z e^{2iE^{-1}t}}{2iE^{-1} D^{\frac{1}{2}} \sinh D^{\frac{1}{2}} h b_3} \times \left( 1 - \frac{a_9 t^{\frac{1}{2}}}{6\sqrt{\pi} b_3} - \frac{t^{\frac{1}{2}}}{\sqrt{\pi} 2iE^{-1}} + \frac{t^{\frac{3}{2}}}{8\sqrt{\pi} E^{-2}} - \frac{a_9 t^{\frac{3}{2}}}{48i b_3 E^{-1} \sqrt{\pi}} + \frac{t^{\frac{3}{2}}}{2\sqrt{\pi}} \frac{a_{10}}{120 b_3} \right)$$

$$(1 - \cosh D^{\frac{1}{2}} h)$$

Expressions for u and v in the clean fluid region consists of rational functions of the hyperbolic terms multiplied by constants involving  $\omega$ , E and D. The transient terms however, decay in time of order  $\frac{4}{\pi^2}$ . It is interesting to observe that in contrast to the single fluid case in the presence of a porous bed, the disturbance does not confine to a layer abutting the boundary. Infact, it is comparatively large outside the layer  $1 - z \leq 1 - h - \left| \omega + 2iE^{-1} \right|^{\frac{1}{2}}$  and within this layer, the disturbance is relatively low, with the velocity vanishing on the boundary plate. We also notice that the velocity field depends on the thickness of the porous layer and the hyperbolic terms occurring in the velocity exponentially decay, provided the thickness of the porous layer is  $h < 1 + \frac{1}{2} E^{\frac{1}{2}}$ . In the absence of porous bed, we observe the formation boundary layer with thickness  $\left| (\omega - 2iE^{-1}) \right|^{\frac{1}{2}}$  near the upper plate and  $\frac{1}{2} E^{\frac{1}{2}}$  near the lower plate. Thus we may conclude that the porous bed in a composite medium prevents formation of boundary layers. Even in the porous bed the hyperbolic terms arising in the solution exhibit that the velocity field is the significantly higher in magnitude in layer  $z > h - [D^{-2} + \left| (\omega - 2iE^{-1})^2 \right|]^{\frac{1}{2}}$  and it gradually dies down in the layer  $z \leq h - [D^{-2} + \left| (\omega - 2iE^{-1})^2 \right|]^{\frac{1}{2}}$ .

#### 4. RESULTS AND DISCUSSION

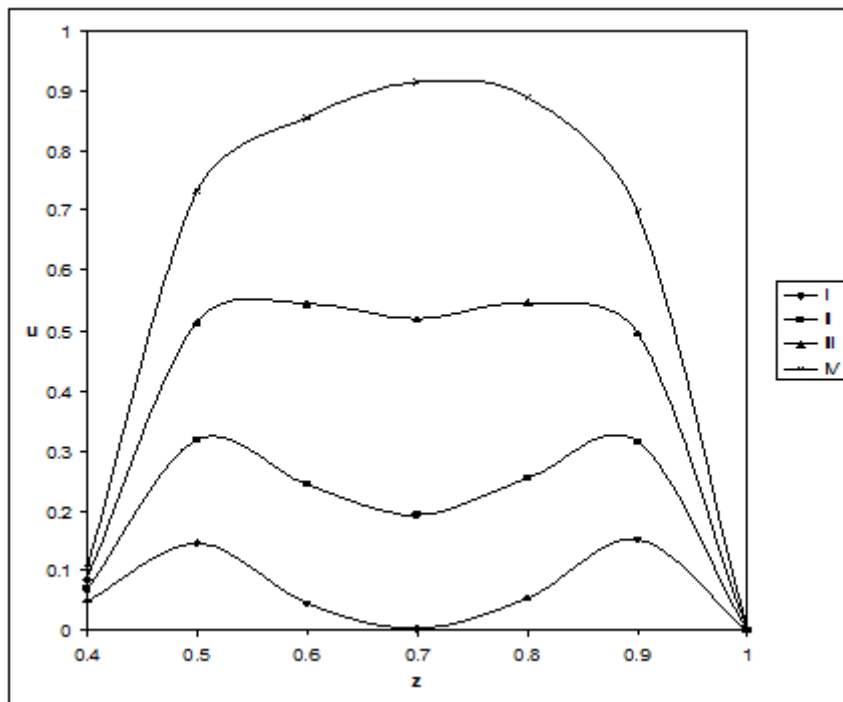
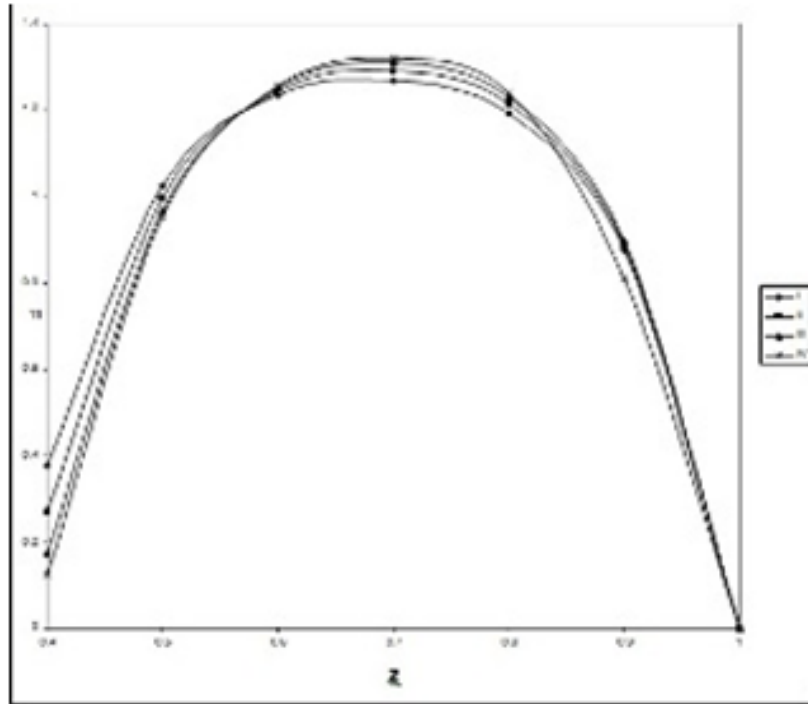


Figure-1: u against E

	I	II	III	IV
E	0.01	0.02	0.03	0.04

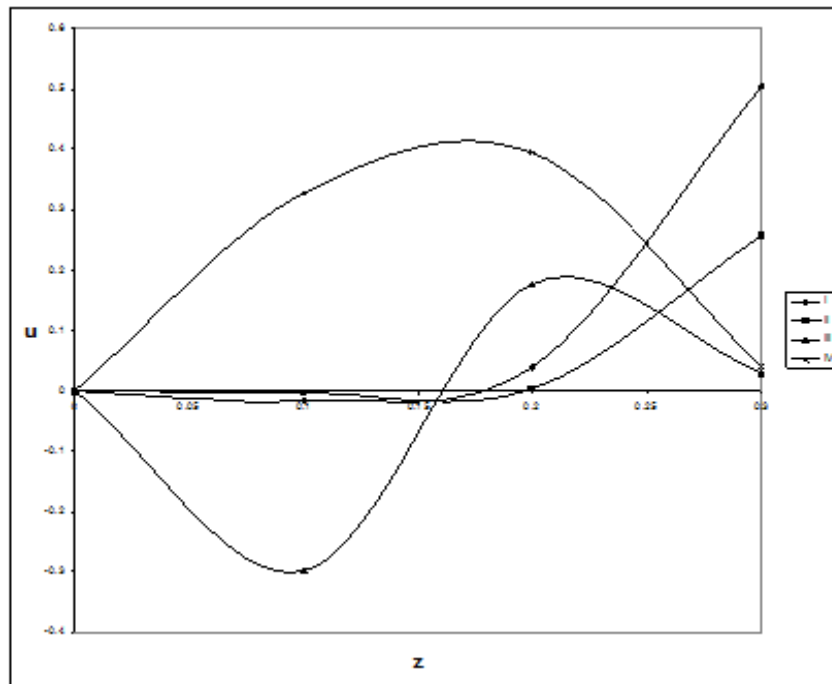
$$D^{-1}=10000, h = 0.4, P = 1, t = 1, w = \frac{\pi}{2}, a=b=1$$



**Figure-2:** u against  $D^{-1}$

	I	II	III	IV
$D^{-1}$	$10^3$	$3 \times 10^3$	$5 \times 10^3$	$10^4$

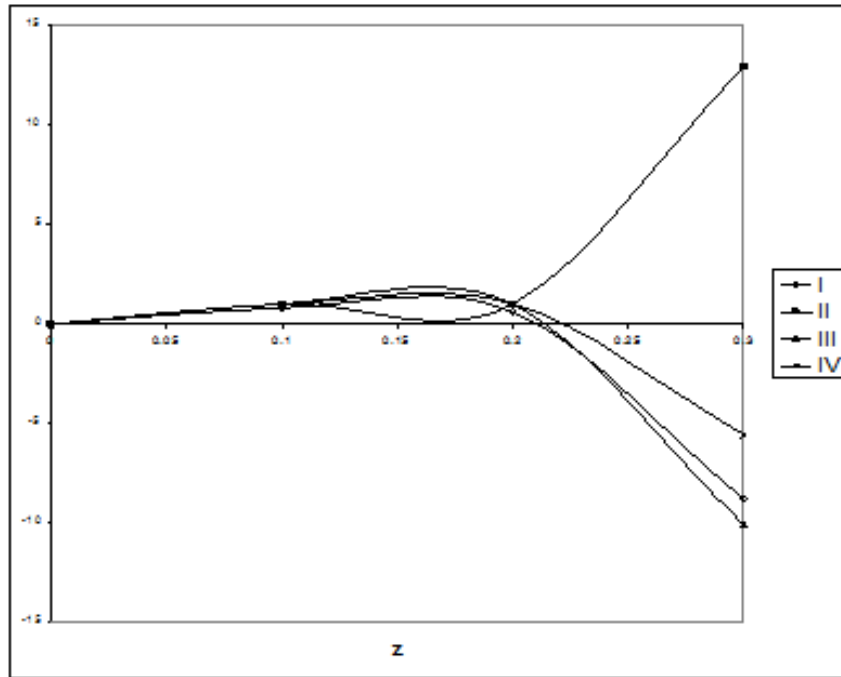
$E=0.05, h = 0.4, P = 1, t = 1, w = \frac{\pi}{2}, a=b=1$



**Figure-3:** u against h

	I	II	III	IV
h	0.2	0.3	0.4	0.5

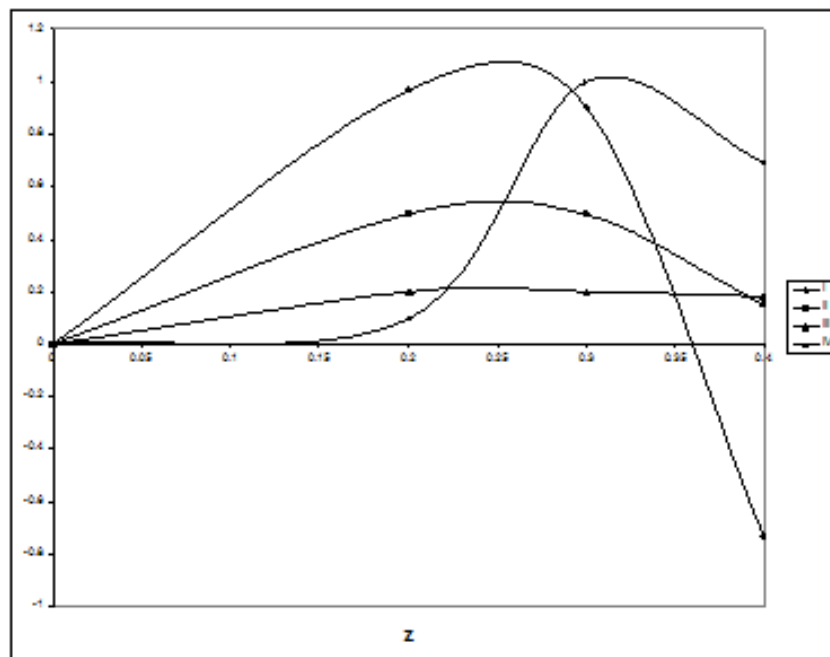
$D^{-1}=10000, E = 0.05, P = 1, t = 1, w = \frac{\pi}{2}, a=b=1$



**Figure-4:**  $u_p$  against E

	I	II	III	IV
E	0.01	0.02	0.03	0.04

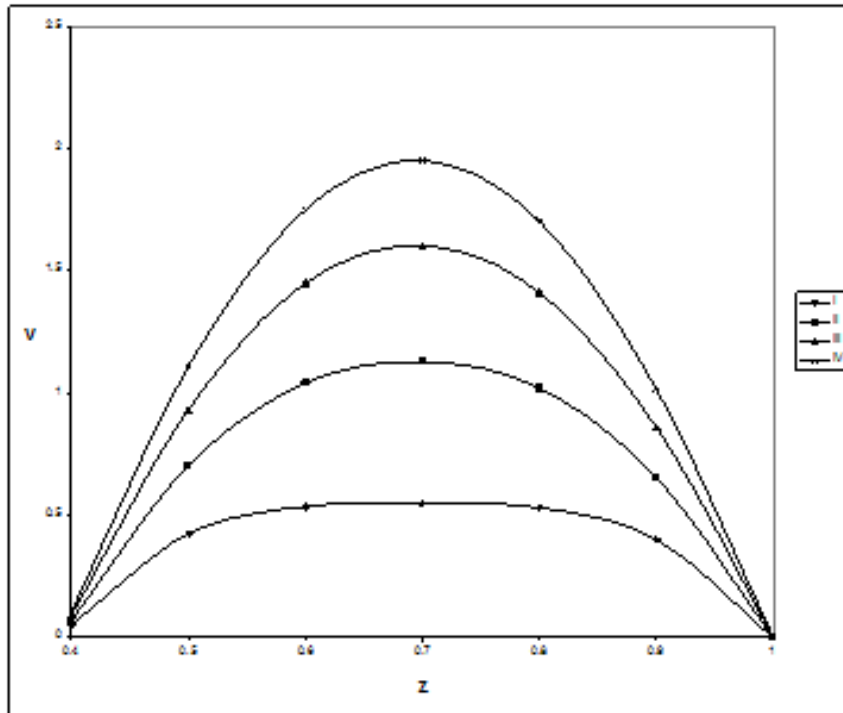
$$D^{-1}=10000, h = 0.4, P = 1, t = 1, w = \frac{\pi}{2}, a=b=1$$



**Figure-5:**  $u_p$  against  $D^{-1}$

	I	II	III	IV
$D^{-1}$	$10^3$	$3 \times 10^3$	$5 \times 10^3$	$10^4$

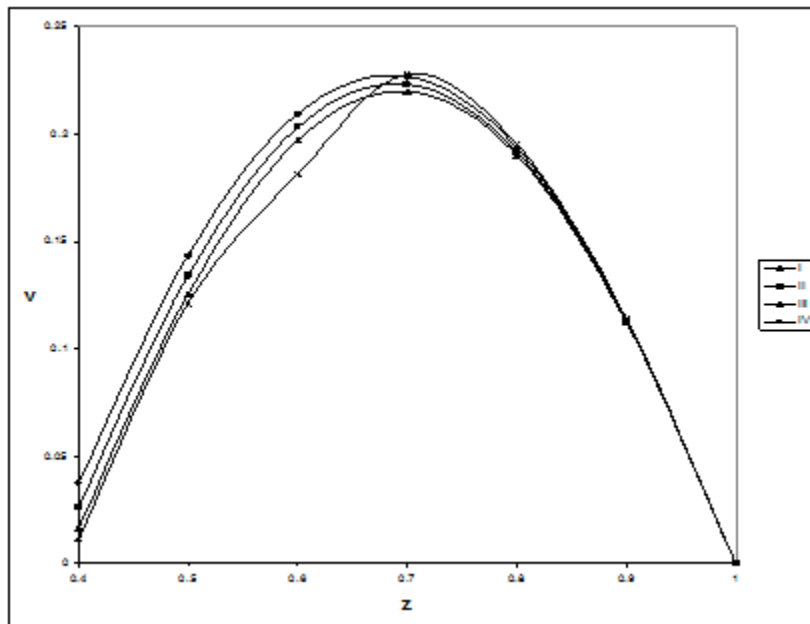
$$E=0.05, h = 0.4, P = 1, t = 1, w = \frac{\pi}{2}, a=b=1$$



**Figure-6:** v against E

	I	II	III	IV
E	0.01	0.02	0.03	0.04

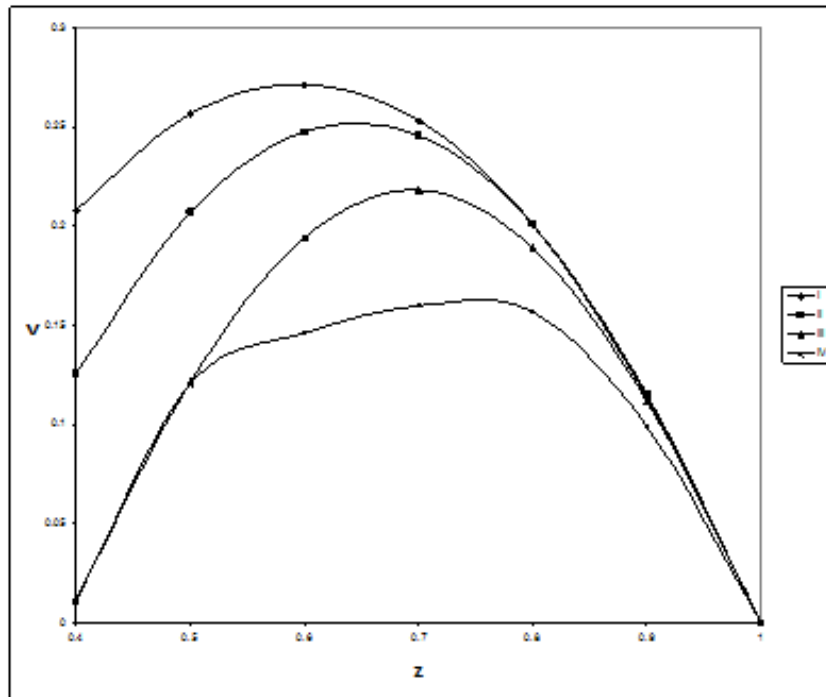
$$D^{-1}=10000, h = 0.4, P = 1, t = 1, w = \frac{\pi}{2}, a=b=1$$



**Figure-7:** v against  $D^{-1}$

	I	II	III	IV
$D^{-1}$	$10^3$	$3 \times 10^3$	$5 \times 10^3$	$10^4$

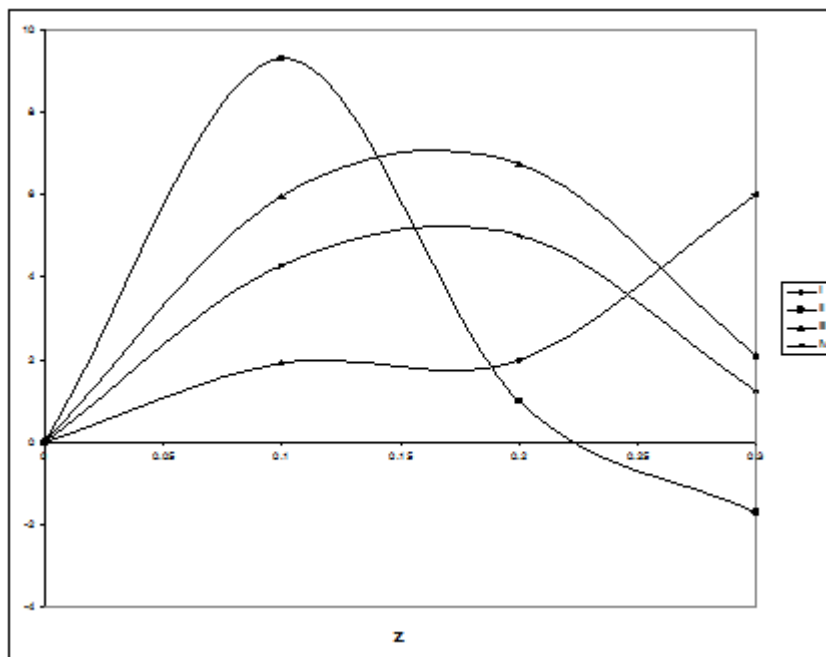
$$E=0.05, h = 0.4, P = 1, t = 1, w = \frac{\pi}{2}, a=b=1$$



**Figure-8:** v against h

	I	II	III	IV
h	0.2	0.3	0.4	0.5

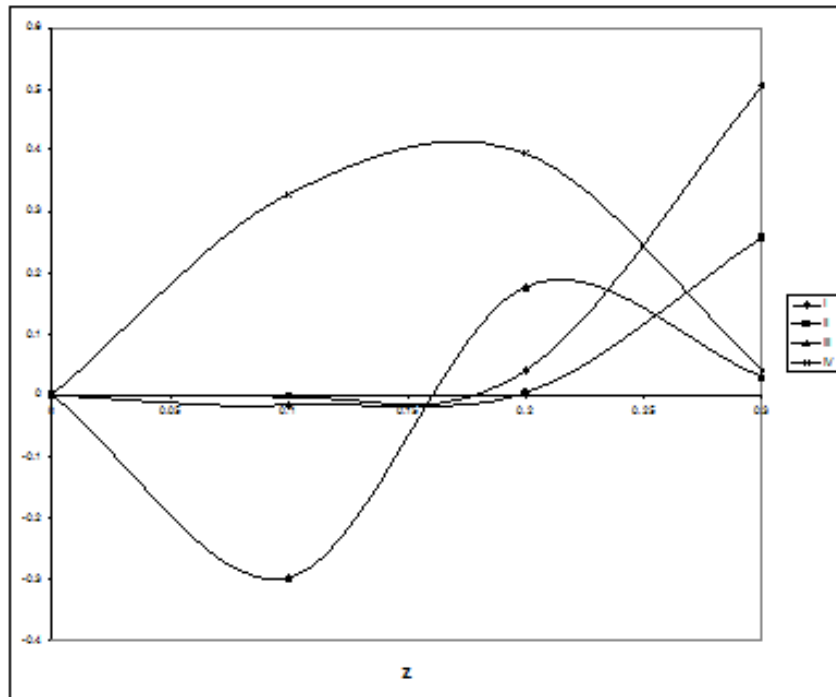
$$D^{-1}=10000, E = 0.05, P = 1, t = 1, w = \frac{\pi}{2}, a=b=1$$



**Figure-9:** v<sub>p</sub> against E

	I	II	III	IV
E	0.01	0.02	0.03	0.04

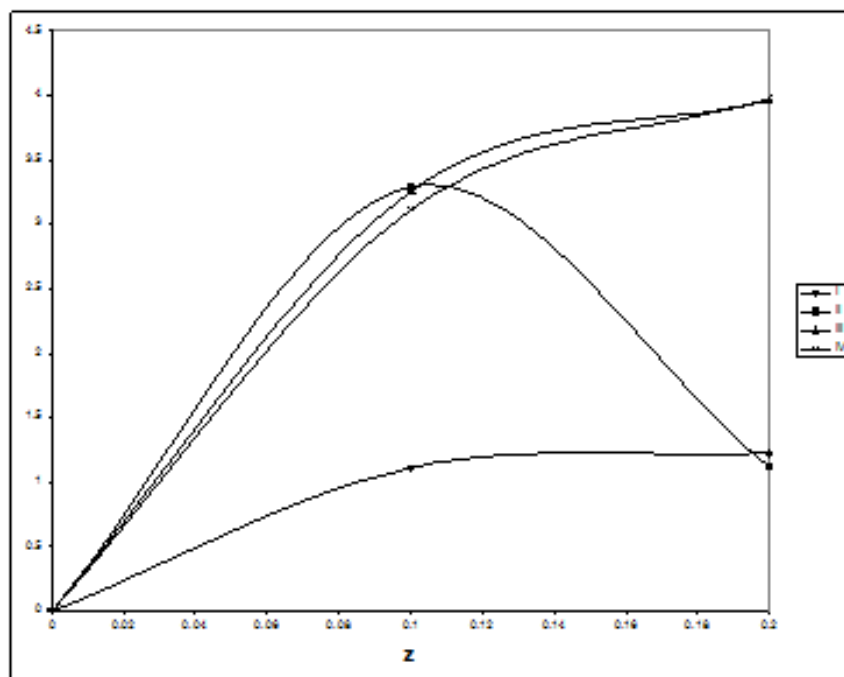
$$D^{-1}=10000, h = 0.4, P = 1, t = 1, w = \frac{\pi}{2}, a=b=1$$



**Figure-10:**  $v_p$  against  $D^{-1}$

	I	II	III	IV
$D^{-1}$	$10^3$	$3 \times 10^3$	$5 \times 10^3$	$10^4$

$E=0.05, h = 0.4, P = 1, t = 1, w = \frac{\pi}{2}, a=b=1$



**Figure-11:**  $v_p$  against  $h$

	I	II	III	IV
$h$	0.2	0.3	0.4	0.5

$D^{-1}=10000, E = 0.05, P = 1, t = 1, w = \frac{\pi}{2}, a=b=1$

The computational analysis has been carried out for variations in the governing parameters  $E$  and  $h$ , in the particular case the boundary plates are at rest. In figures 1, 2, 3 correspond to profiles  $u$  with reference to  $E, D^{-1}, h$ . We notice that the effect of  $E$  is significant on  $u$ , with the magnitude of  $u$  increasing with  $E$ . Thus the rotation affects the clean fluid in comparison to the porous medium. (fig.1). Also from fig.2, we find that  $u$  increases with increasing  $D^{-1}$  i.e., lesser the permeability of the porous bed the higher the magnitude of the clean fluid region. This is in contrast to behaviour of the corresponding velocity,  $u_p$  in the porous bed (fig. 5), where  $u_p$  reduces with  $D^{-1}$ . Thus in a densely porous bed the fluid moves with reduced velocity (fig. 5). However with reference to variation in  $E$ , the behavior of  $u_p$  in the porous bed is similar that of  $u$  with  $u$  enhancing with  $E$ . (fig. 4). The thickness of porous bed influence of the flow in the clean fluid region, we observe that the velocity  $u$  enhances with increasing the thickness of the bed (fig. 3).

The magnitude of  $v_p$  in the porous bed is very low compare to it corresponding value in the clean fluid region. (figs (6-11)). In the porous regions  $v_p$  decays the faster with increasing the  $D^{-1}$  and at  $D^{-1}$  is of order  $10^4$ ,  $v_p$  is almost negligible and does not exhibit variation with other parameters (fig 9-11). In the clean fluid region,  $v$  increases with increase in  $E$  (fig. 6). We notice that  $v$  reduces with increase  $D^{-1}$  (fig. 7) i.e., lesser the permeability lesser magnitude of  $V$ , although the depreciation is relatively to low compare to its enhancement with  $E$ . (fig 6&7). We also notice that increasing the thickness of porous bed reduces  $V$  in the clean fluid region (fig. 8).

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