

**THERMAL CONDUCTIVITY  
FOR HEAT AND MASS TRANSFER FLOW PAST AN INFINITE VERTICAL**

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**ABSTRACT**

*This paper investigates the flow and heat mass transfer past an infinite vertical plate with variable thermal conductivity, heat source and chemical reaction. The consequential equations are discredited by means of Laplace transform with boundary condition and solved numerically. The velocity, temperature and concentration profiles are presented graphically. This investigation is undertaken to study the heat and accumulation transport flow precedent an endless vertical plate with variable thermal conductivity. The governing equations for the model are formulated with appropriate boundary conditions. The flow phenomenon are characterized by the flow parameters such as Prandtl number ( $Pr$ ), Schmidt number ( $Sc$ ), Eckert number ( $Ec$ ), magnetic field ( $M$ ), porosity ( $K$ ), thermal Grashof number ( $Gr$ ), mass Grashof number ( $Gc$ ), radiation ( $N$ ), suction ( $\alpha$ ), thermal conductivity ( $\tau$ ), chemical reaction ( $Kr$ ) and reaction order ( $n$ ) which are studied for speed field, high temperature field and attentiveness allocation accessible graphically. Keywords Heat Transfer, Mass Transfer, Thermal Conductivity, V Keywords - Heat Transfer, Mass transport, changeable Thermal Conductivity, Heat Source, perpendicular Plate*

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**INTRODUCTION**

In nuclear manufacturing, cooling of intermediate is additional significant beginning the security position of view and throughout this cooling procedure the cover high temperature starts oscillate about a non-zero constant mean temperature. The oscillatory flow has application in industrial and aerospace engineering. In the processes involving high temperatures, the radiation heat transfer in combination with conduction, convection and also mass transfer plays very significant role in the intend of applicable equipments in the areas such as nuclear power plants, gas turbines and the various propulsion devices for aircrafts, missiles, satellites and space vehicles. Moreover, radiation effect is significant in the dynamics of fluid in chemical, environmental, mechanical and solar power engineering. Thus,

Although different authors studied heat and mass transfer with or without radiation and viscous dissipation effects on the flow past an infinite vertical plate by considering different surface conditions but the learn on the effects of radiation on free convection high temperature and mass move with unstable thermal conductivity, viscous dissipation and reaction order on flow standard an endless vertical plate has not been found in the literature and consequently the motivation to undertake. Heat and mass transfer flow past an infinite vertical plate with variable thermal conductivity.

**2. REVIEW OF LITERATURE**

- ❖ Muthucumaraswamy and Senthil Kumar [1] the heat and mass transfer effects on moving vertical plate in the presence of thermal radiation.
- ❖ Gupta *et al.* [2] Heat and mass transfer on a stretching sheet with suction or blowing.
- ❖ Sattar [3] the free of charge convection and accumulation transfer flow from side to side a absorbent medium precedent an endless perpendicular absorbent plate by time independent temperature and concentration.
- ❖ Israel-Cookey *et al.* [4] the pressure of viscous dissipation and radiation on trembling MHD free convection flow past an infinite heated vertical plate in a porous medium with time dependent suction.
- ❖ Soundalgekar *et al.* [7] the effects of viscous dissipative heat on the transient free convection flow past an infinite vertical plate with a step change in plate temperature. The problem governed by nonlinear coupled partial differential equations was solved by finite difference method. Buoyancy is also of importance in an environment where differences between land and air temperatures can give rise to complicated flow patterns.
- ❖ Chamkha [13] studied the effects of solar radiation on free convection in an isotropic, consistent porous average support by a perpendicular level cover by a computational method.

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- ❖ Sangapatnam *et al.* [14]: considered the emission and mass transfer effects on MHD free convection flow past impulsively-started isothermal vertical plate with dissipation.
- ❖ Yasar and Moses [15] developed a one-dimensional adaptive-grid finite-differencing computer code for thermal radiation magneto hydro dynamic (RMHD) simulations of fusion plasmas.

Aboeldahab and Azzam [16] described the effects of magnetic field on hydro magnetic mixed free-forced heat and mass convection of a gray, optically-thick, electrically conducting viscous liquid the length of a semi-infinite disposed cover for high temperature and attentiveness..

## 2. PROBLEM FORMULATION

1. An unsteady endless perpendicular isothermal absorbent cover of laminar natural convection flow of dissipative and searing liquid in the attendance of oblique magnetic field surrounded on one side by infinite mass of fluid like air or water and both at same temperature  $T'_\infty$  and the mass concentration  $C'_\infty$  initially.
2. At time  $t' > 0$ , the plate temperature and the mass concentration is raised to  $T'_w$  and  $C'_w$ ,
3. Causing the presence of high temperature and concentration difference  $T'_w - T'_\infty$  and  $C'_w - C'_\infty$  respectively.
4. As the plate is infinite in extent, the physical variables are functions of  $y'$  and  $t'$  where  $y'$  is taken normal to the plate and the  $x'$ -axis is taken along the plate in the vertically upward direction. Under the Boussinesq approximation,
5. The governing equations for the flow are continuity, momentum, mass concentration and energy respectively are

$$\frac{\partial u'}{\partial t'} = g\beta(T' - T'_\infty) + g\beta^*(C' - C'_\infty) + \nu \frac{\partial^2 u'}{\partial y'^2} - \frac{\sigma B_0^2}{\rho} u' \quad (1)$$

$$\rho C_p \frac{\partial T'}{\partial t'} = k \frac{\partial^2 T'}{\partial y'^2} \quad (2)$$

$$\frac{\partial C'}{\partial t'} = D \frac{\partial^2 C'}{\partial y'^2} - K_1 C' \quad (3)$$

$$\begin{aligned} u' = 0, \quad T' = T'_\infty, \quad C' = C'_\infty, \quad \text{for all } y' \text{ and } t' \leq 0 \\ u' = U_0, \quad T' = T'_\infty + (T'_w - T'_\infty)At', \quad C' = T'_w \text{ at } y' = 0 \\ u' \rightarrow 0, \quad T' \rightarrow T'_\infty, \quad C' \rightarrow C'_\infty, \quad \text{as } y' \rightarrow \infty, \quad t > 0 \end{aligned} \quad (4)$$

The initial and boundary conditions relevant to the fluid flow are:

$$\begin{aligned} u = \frac{u'}{U_0}, \quad t = \frac{t'U_0^2}{\nu}, \quad y = \frac{y'U_0}{\nu}, \quad \theta = \frac{T' - T'_\infty}{T'_w - T'_\infty}, \\ \phi = \frac{C' - C'_\infty}{C'_w - C'_\infty}, \quad Gr = \frac{g\beta\nu(T'_w - T'_\infty)}{U_0^3}, \\ Gm = \frac{g\beta^*\nu(C'_w - C'_\infty)}{U_0^3}, \quad Pr = \frac{\mu C_p}{k}, \\ R = \frac{\nu K_1}{U_0^2}, \quad Sc = \frac{\nu}{D}, \quad M = \frac{\sigma B_0^2 \nu}{\rho U_0^2} \end{aligned} \quad (5)$$

where

- $\nu$  = kinematic viscosity of the grey fluid,
- $\sigma$  = Stefan-Boltzmann constant,
- $B_0$  = constant magnetic field intensity,
- $\rho$  = density,
- $K^*$  = permeability,
- $g$  = gravitational constant,
- $\beta$  = thermal expansion coefficient,
- $\beta^*$  = concentration expansion coefficient,
- $T' = t$  = temperature,
- $c'$  = mass concentration,
- $D$  = chemical molecular diffusivity,
- $R^*$  = chemical reaction,
- $k_0$  = mean absorption coefficient of thermal expansion,

- $C'$  = heat capacity at constant pressure,
- $q_r$  = radioactive heat flux,
- $u'$  and  $v'$  are velocity components in x and y directions respectively,
- $K(T)$  = thermal conductivity,
- $T_w$  = wall temperature,
- $T_\infty$  = free stream temperature,
- $C_w$  = species concentration at the plate surface,
- $C_\infty$  = free stream concentration.

Quantities (5), the equation (1), (2), and (3) then reduce to the following forms

$$\frac{\partial u}{\partial t} = \frac{\partial^2 u}{\partial y^2} + Gr\theta + Gm\phi - Mu \tag{6}$$

$$\frac{\partial \theta}{\partial t} = \frac{1}{Pr} \frac{\partial^2 \theta}{\partial y^2} \tag{7}$$

$$\frac{\partial \phi}{\partial t} = \frac{1}{Sc} \frac{\partial^2 \phi}{\partial y^2} - R\phi \tag{8}$$

### 3. ANALYTICAL SOLUTION

To solve the governing equations in dimensionless form, we introduce the following non-dimensional quantities:

$$\left. \begin{aligned} u = 0, & \quad \theta = 0, & \quad \phi = 0, \text{ for all } y \text{ and } t \leq 0 \\ u = 1, & \quad \theta = t, & \quad \phi = 1, \text{ at } y = 0 \\ u \rightarrow 0, & \quad \theta \rightarrow 0, & \quad \phi \rightarrow 0, \text{ as } y \rightarrow \infty \end{aligned} \right\}, t > 0 \tag{9}$$

The governing equations on using (9) into (1), (2), (3), (5) and using (6) to (9) into (4) reduce to the following

$$\theta(y,t) = \left( t + \frac{y^2 Pr}{2} \right) \operatorname{erfc} \left( \frac{y\sqrt{Pr}}{2\sqrt{t}} \right) - \frac{y\sqrt{t} Pr}{\sqrt{\pi}} e^{-\frac{y^2 Pr}{4t}} \tag{10}$$

$$\phi(y,t) = \frac{1}{2} \left\{ e^{-y\sqrt{ScR}} \operatorname{erfc} \left( \frac{y\sqrt{Sc}}{2\sqrt{t}} - \sqrt{Rt} \right) + e^{y\sqrt{ScR}} \operatorname{erfc} \left( \frac{y\sqrt{Sc}}{2\sqrt{t}} + \sqrt{Rt} \right) \right\} \tag{11}$$

$$\begin{aligned} u(y,t) = & \frac{G_4}{2} \left\{ e^{-y\sqrt{M}} \operatorname{erfc} \left( \frac{y}{2\sqrt{t}} - \sqrt{Mt} \right) + e^{y\sqrt{M}} \operatorname{erfc} \left( \frac{y}{2\sqrt{t}} + \sqrt{Mt} \right) \right\} \\ & + \frac{yG_1}{4b\sqrt{M}} \left\{ e^{-y\sqrt{M}} \operatorname{erfc} \left( \frac{y}{2\sqrt{t}} + \sqrt{Mt} \right) - e^{y\sqrt{M}} \operatorname{erfc} \left( \frac{y}{2\sqrt{t}} - \sqrt{Mt} \right) \right\} \\ & + \frac{G_1}{2b^2} \left[ e^{bt} \left\{ \left\{ e^{-y\sqrt{c}} \operatorname{erfc} \left( \frac{y}{2\sqrt{t}} - \sqrt{ct} \right) + e^{y\sqrt{c}} \operatorname{erfc} \left( \frac{y}{2\sqrt{t}} + \sqrt{ct} \right) \right\} \right. \right. \\ & \left. \left. - \left\{ e^{-y\sqrt{bPr}} \operatorname{erfc} \left( \frac{y\sqrt{Pr}}{2\sqrt{t}} - \sqrt{bt} \right) + e^{y\sqrt{bPr}} \operatorname{erfc} \left( \frac{y\sqrt{Pr}}{2\sqrt{t}} + \sqrt{bt} \right) \right\} \right\} \right] \\ & + \frac{G_2}{2d} e^{dt} \left[ \left\{ e^{-y\sqrt{k}} \operatorname{erfc} \left( \frac{y}{2\sqrt{t}} - \sqrt{kt} \right) + e^{y\sqrt{k}} \operatorname{erfc} \left( \frac{y}{2\sqrt{t}} + \sqrt{kt} \right) \right\} \right. \\ & \left. - \left\{ e^{-y\sqrt{hSc}} \operatorname{erfc} \left( \frac{y\sqrt{Sc}}{2\sqrt{t}} - \sqrt{ht} \right) + e^{y\sqrt{hSc}} \operatorname{erfc} \left( \frac{y\sqrt{Sc}}{2\sqrt{t}} + \sqrt{ht} \right) \right\} \right. \\ & \left. + \left\{ e^{-y\sqrt{ScR}} \operatorname{erfc} \left( \frac{y\sqrt{Sc}}{2\sqrt{t}} - \sqrt{Rt} \right) + e^{y\sqrt{ScR}} \operatorname{erfc} \left( \frac{y\sqrt{Sc}}{2\sqrt{t}} + \sqrt{Rt} \right) \right\} \right] \end{aligned}$$

$$+ \frac{G_1}{b} \left[ \left( t + \frac{y^2 \text{Pr}}{2} \right) \text{erfc} \left( \frac{y\sqrt{\text{Pr}}}{2\sqrt{t}} \right) - \frac{y\sqrt{t\text{Pr}}}{\sqrt{\pi}} e^{-\frac{y^2 \text{Pr}}{4t}} \right] + \frac{G_3}{2} \text{erfc} \left( \frac{y\sqrt{\text{Pr}}}{2\sqrt{t}} \right) \quad (12)$$

subject to the boundary conditions

$$b = \frac{M}{\text{Pr}-1}, c = M + b, d = \frac{RSc - M}{1 - Sc}, h = R + d,$$

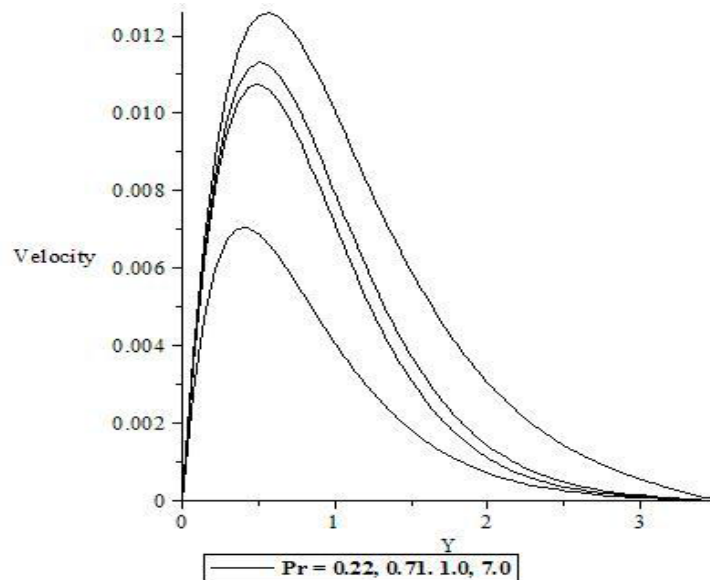
$$k = m + d, G_1 = \frac{Gr}{\text{Pr}-1}, G_2 = \frac{Gm}{Sc - 1},$$

$$G_3 = 1 - \frac{G_2}{d} - \frac{G_1}{b^2}, G_4 = G_3 - \frac{tG_1}{b} \quad (13)$$

where Pr is the Prandtl number, Sc is Schmidt number, Ec is Eckert number, Gr is thermal Grashof number, Gc is mass Grashof number, and M is magnetic field, K is porosity, N is the radiation, α is suction, τ is the thermal conductivity, Kr is the chemical reaction and n is reaction order parameters.

#### 4. RESULTS AND DISCUSSIONS

1. The numerical solutions are simulated for different values of the Prandtl number Pr, Schmidt number Sc, Eckert number Ec, thermal Grashof number Gr, mass Grashof number Gc, radiation parameter N, magnetic field parameter M, porosity parameter K, thermal conductivity parameter τ, suction parameter α, reaction order parameter n and chemical reaction parameter Kr.
2. The following parameters values are fixed throughout the calculations except where otherwise stated, Pr = 0.71, Sc = 0.62, Ec = 0.01, M = 5.0, K = 1.0, Gr = 0.1, Gc = 0.1, N = 1.0, α = 0.2, τ = 1.0, Kr = 0.5, n = 1.0, t = 0.5, y = 0.3.5.



**Figure 1:** Variation of Velocity against y for different values of Pr.

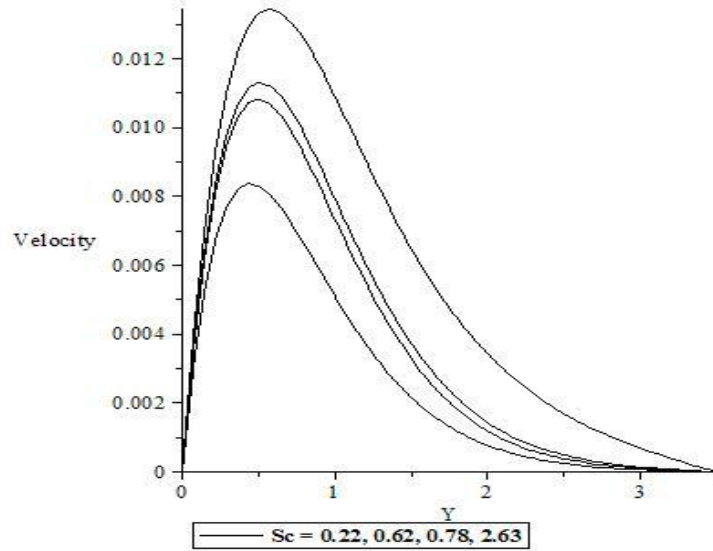


Figure 2: Variation of Velocity against y for different values of Sc.

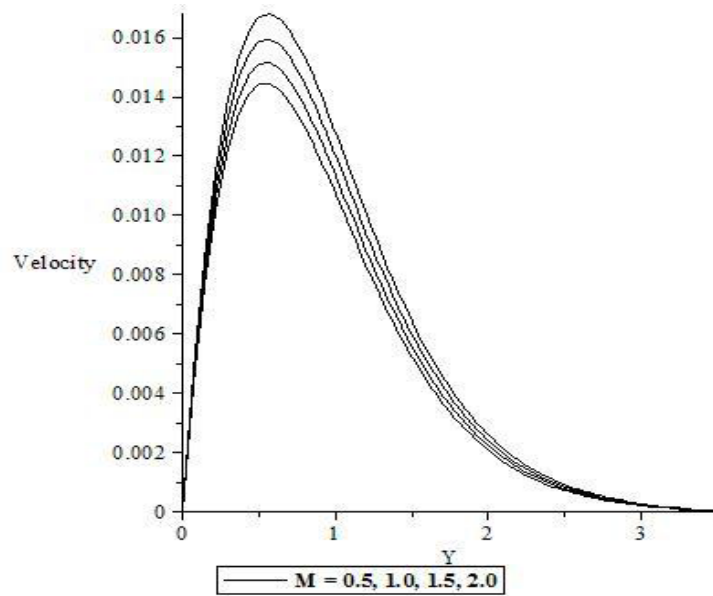


Figure 3: Variation of Velocity against y for different values of M.

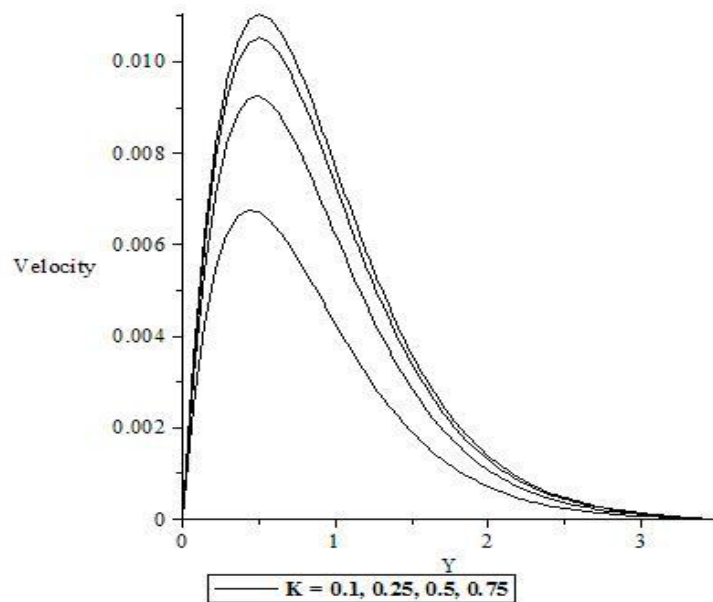


Figure 4: Variation of Velocity against y for different values of K.

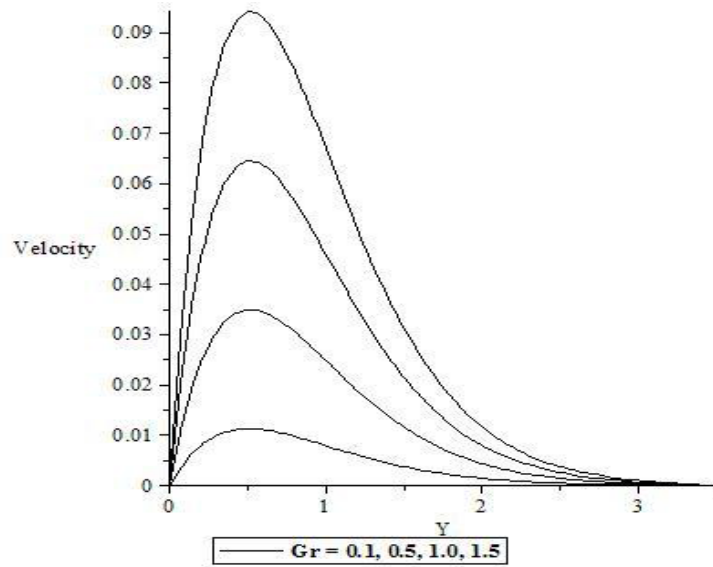


Figure 5: Variation of Velocity against y for different values of Gr.

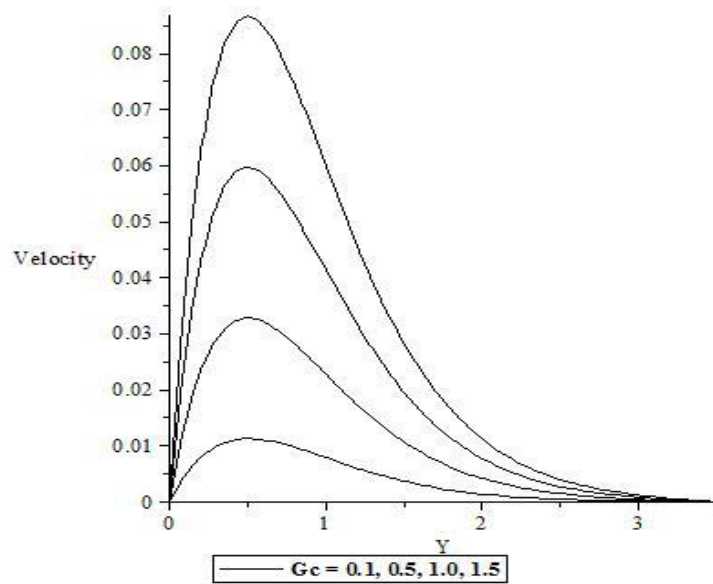


Figure 6: Variation of Velocity against y for different values of Gc.

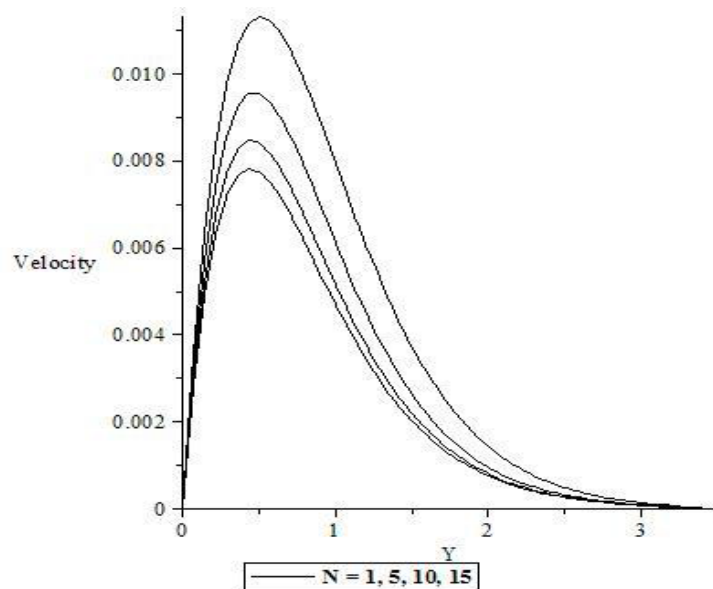


Figure 7: Variation of Velocity against y for different values of N.

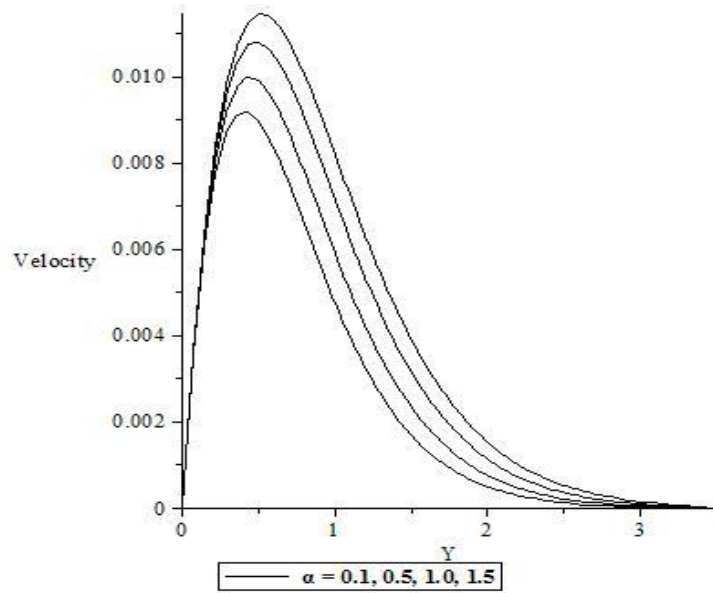


Figure 8: Variation of Velocity against y for different values of  $\alpha$ .

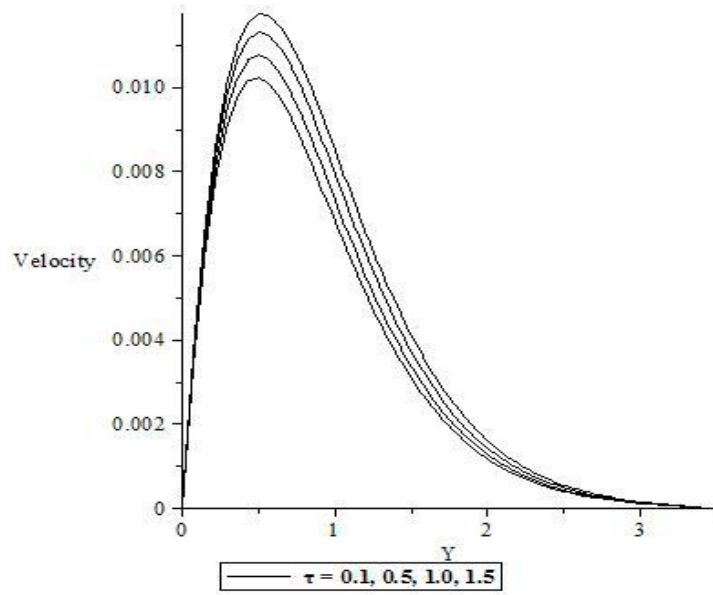


Figure 9: Variation of Velocity against y for different values of  $\tau$ .

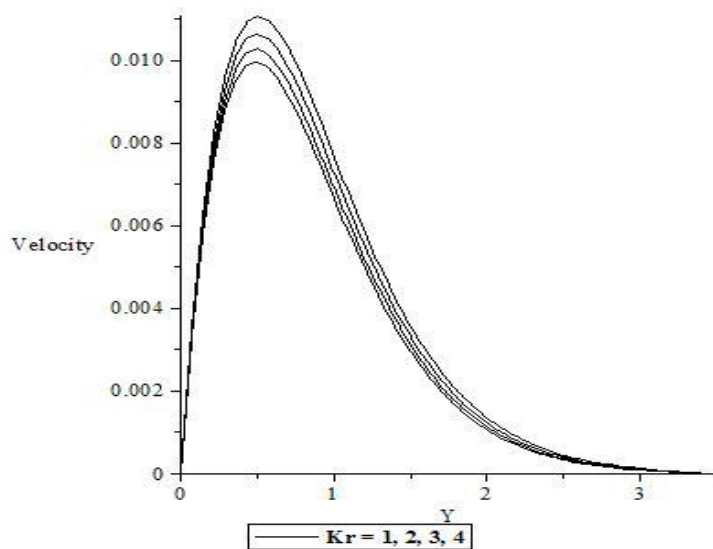


Figure 10: Variation of Velocity against y for different values of Kr.

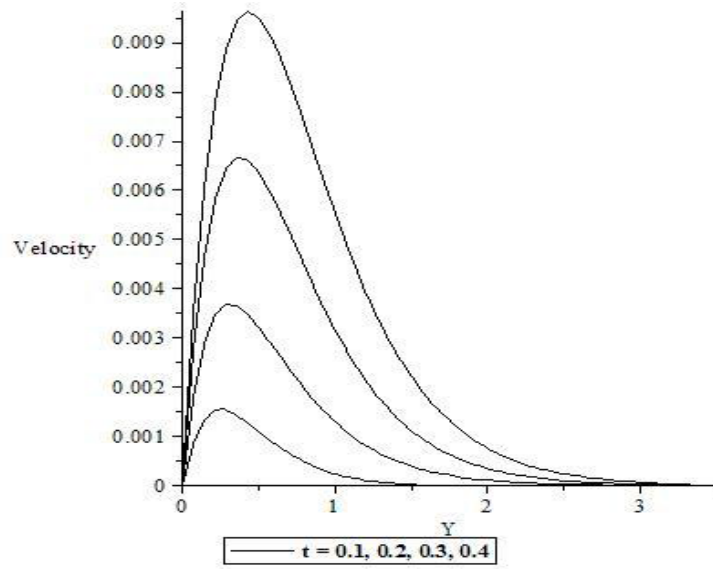


Figure 11: Variation of Velocity against  $y$  for different values of  $t$ .

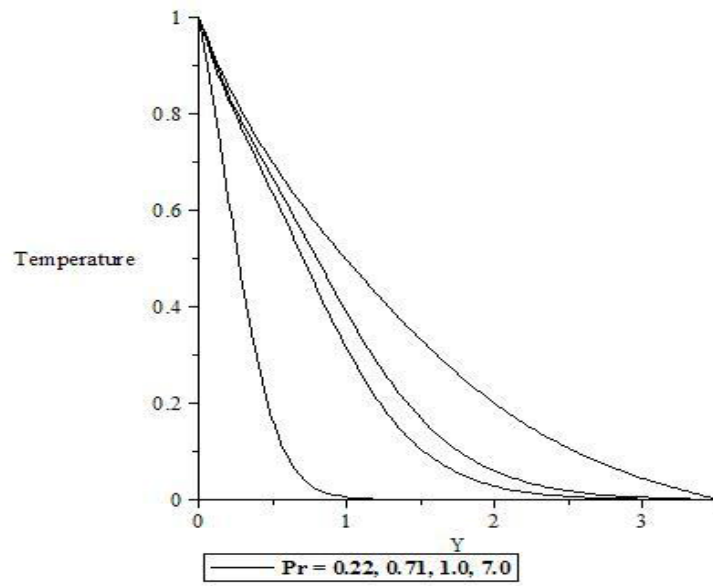


Figure 12: Variation of Temperature against  $y$  for different values of  $Pr$ .

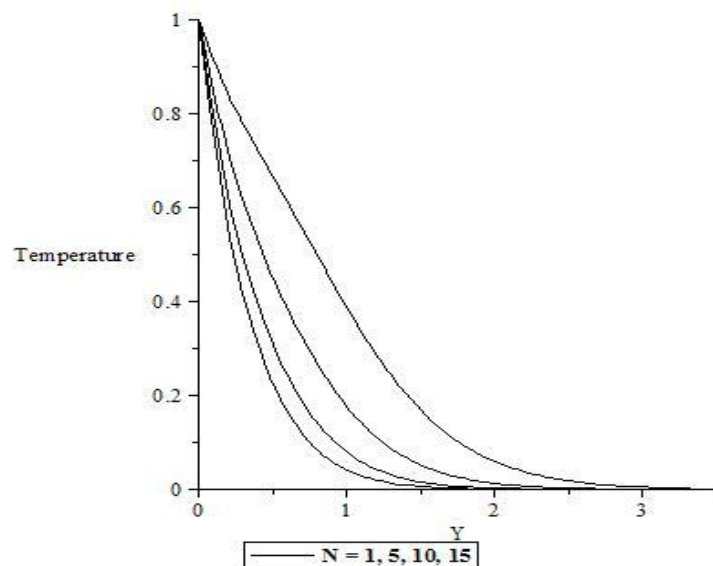


Figure 13: Variation of Temperature against  $y$  for different values of  $N$ .



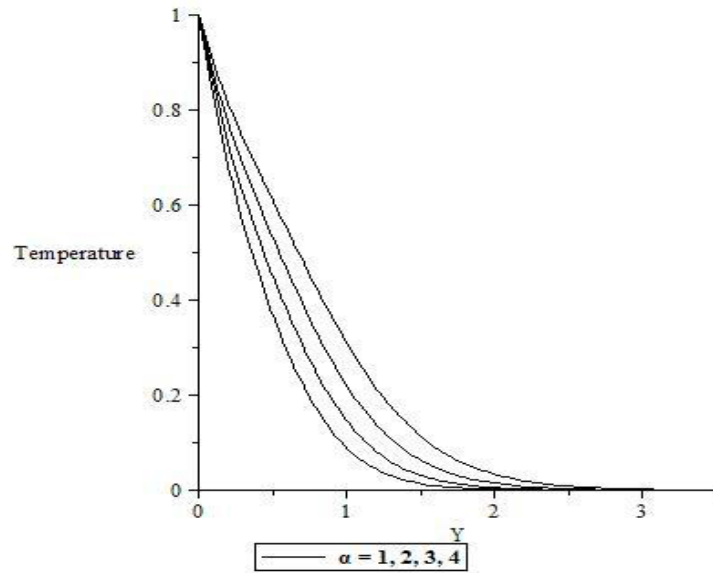


Figure 14: Variation of Temperature against y for different values of  $\alpha$ .

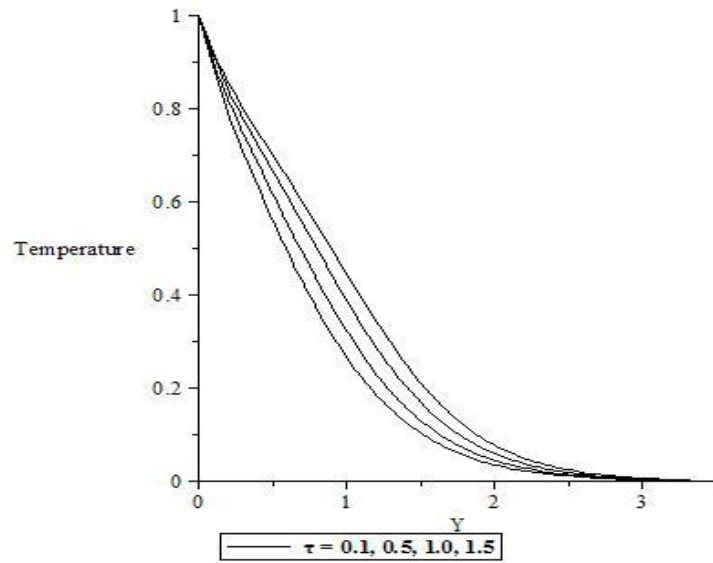


Figure 15: Variation of Temperature against y for different values of  $\tau$ .

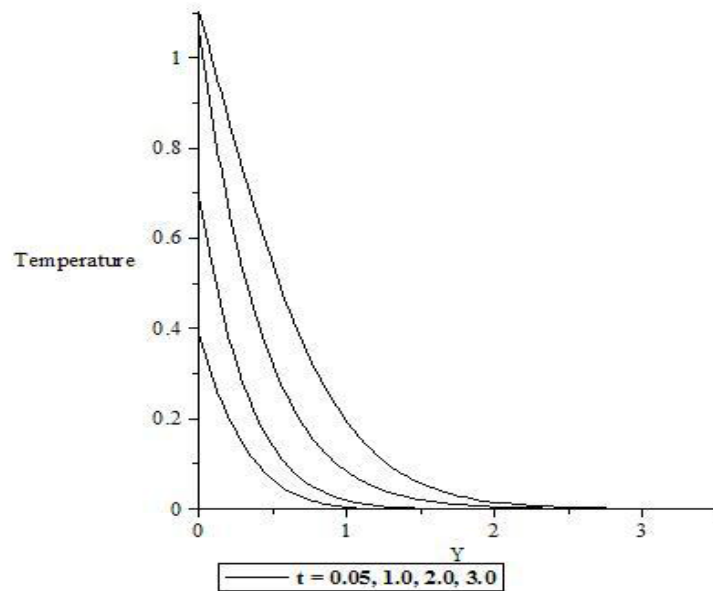


Figure 16: Variation of Temperature against y for different values of  $t$ .

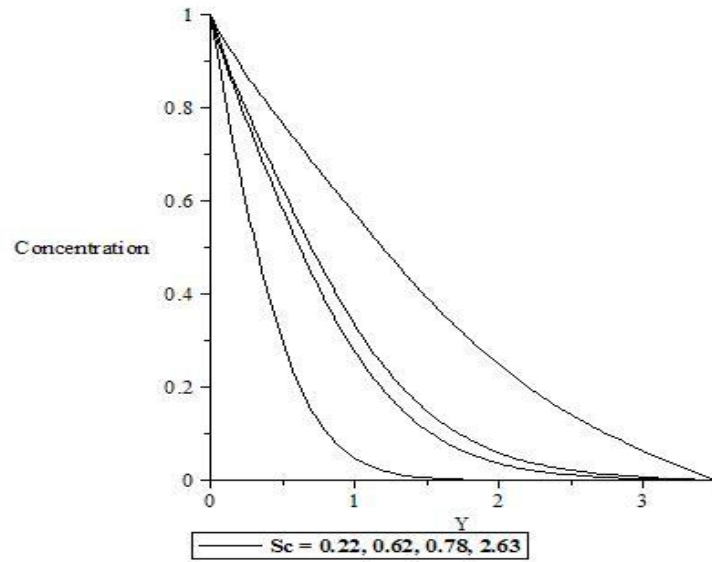


Figure 17: Variation of Concentration against  $y$  for different values of  $Sc$ .

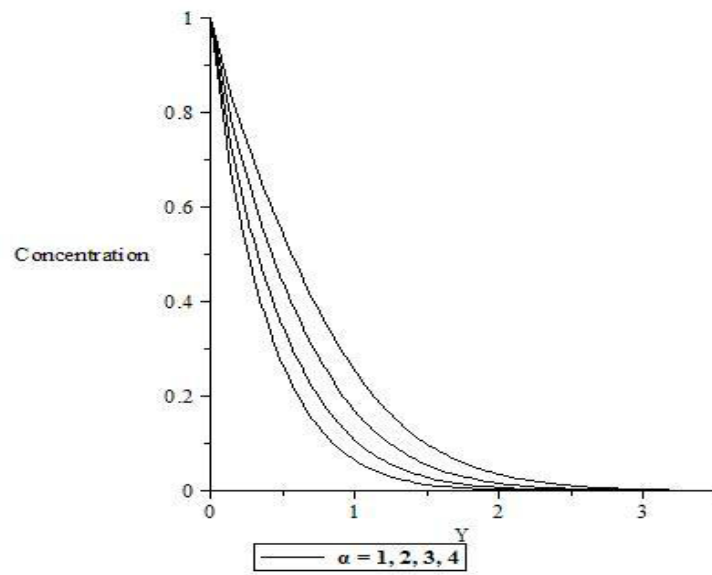


Figure 18: Variation of Concentration against  $y$  for different values of  $\alpha$ .

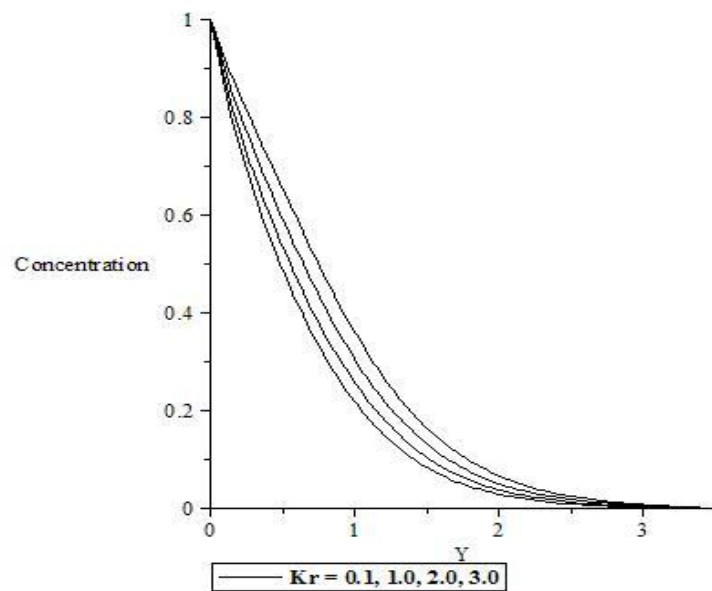


Figure 19: Variation of Concentration against  $y$  for different values of  $Kr$ .

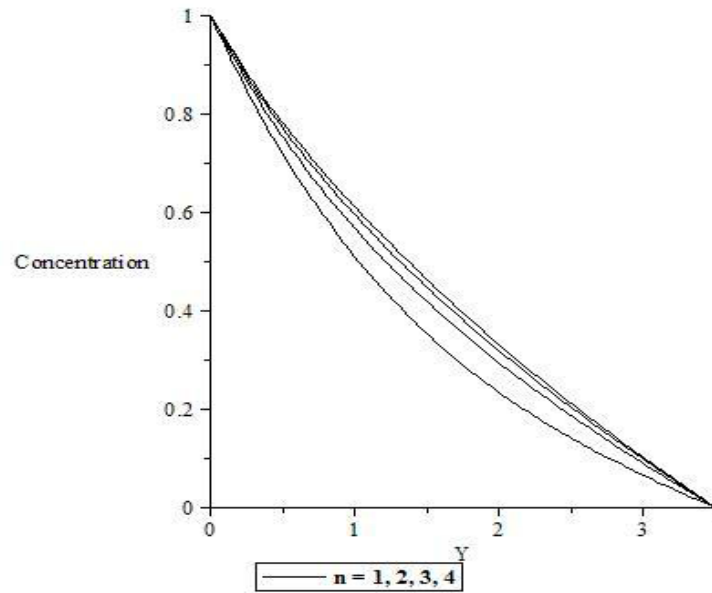


Figure 20: Variation of Concentration against y for different values of n.

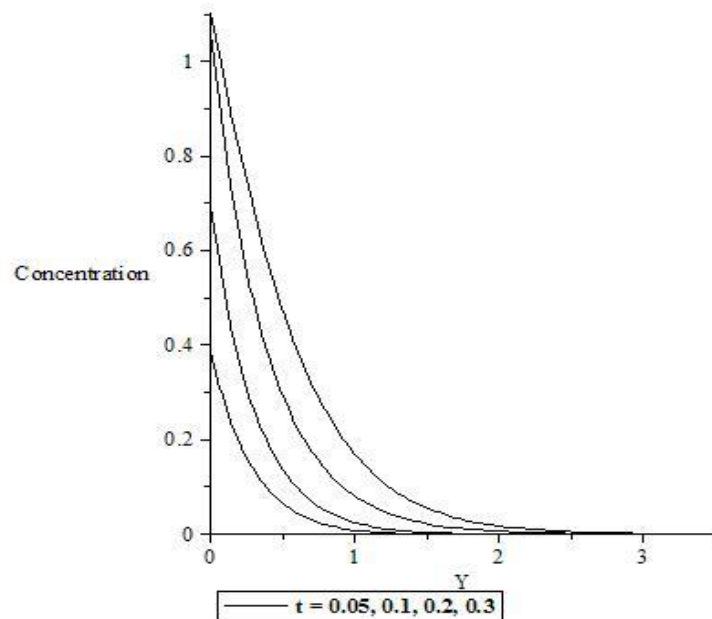


Figure 21: Variation of Concentration against y for different values of t.

## 5. CONCLUSIONS

- The speed enlarges with augment in the thermal Grashof number, mass Grashof number, thermal conductivity parameter, porosity parameter and time. Whereas the velocity decrease with increasing Prandtl number, Schmidt number, magnetic field parameter, radiation parameter, suction parameter and chemical reaction parameter.
- The high temperature augments with augment in thermal conductivity parameter and time. But, the temperature decrease with increasing Prandtl number and suction parameter.
- The concentration increase with increasing reaction order parameter and time while the concentration decrease with increase in Schmidt number, suction parameter and chemical reaction parameter.

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