

SIMULTANEOUS EFFECTS OF HALL CURRENT THERMAL DIFFUSION AND CHEMICAL REACTION ON MHD CONVECTION FLOW PAST A VERTICAL PLATE

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ABSTRACT

The objective of this paper is to investigate the combined effects of Hall current, thermal diffusion and chemical reaction effects on MHD free convective flow past a vertical porous plate with heat and mass transfer. Here we considered Darcy resistance into account and constant permeability of the medium numerically and neglecting induced magnetic field in comparison to applied magnetic field. The momentum, energy, and concentration equations derived as coupled second-order, ordinary differential equations and are solved numerically using a highly accurate and thoroughly tested finite element method (FEM). The velocity, temperature and concentration profiles are presented graphically

Keywords: MHD flow, porous medium, Thermal diffusion, Finite element method.

INTRODUCTION

Free convection flows past a vertical surface or plate were studied extensively in the literature due to its applications in engineering and environmental processes. The heating of rooms and buildings by the use of radiators is a familiar example of heat transfer by free convection. Heat losses from hot pipes, ovens etc surrounded by cooler air, are at least in part, due to free convection. The problem of heat transfer in a vertical channel has been studied in recent years as a model for the re-entry problem. This is due to the significant role of thermal radiation in surface heat transfer when convection heat transfer is similar, particularly in free convection problems involving absorbing emitting fluids. In view of these applications many researchers have studied MHD free convective heat and mass transfer flow in a porous medium, some of them are Raptis and Kafoussias [1].

The Hall effect is the making of a voltage difference across an electrical conductor, transverse to an electric current in the conductor and an electromagnetic field is perpendicular to the current. It is found by Edwin Hall. The current development of magnetohydrodynamics application is toward a strong magnetic field and toward a low density of the gas. Under this condition, the Hall current becomes important. That importance studied by many researchers. Recently Srinivasa raju *et al.* [2] analyzed the influence of hall current, thermal diffusion and diffusion thermo on magnetohydrodynamic fluid flow past an infinite moving vertical plate using finite element method.

Ming-chun *et al.* [3] took an account of the thermal diffusion and diffusion-thermo effects, to study the properties of the heat and mass transfer in a strongly endothermic chemical reaction system for a porous medium. Gaikwad *et al.* [4] investigated the onset of double diffusive convection in a two component couple of stress fluid layer with Soret and Dufour effects using both linear and non-linear stability analysis. Osalusi *et al.* [5] investigated thermo-diffusion and diffusion-thermo effects on combined heat and mass transfer of a steady hydromagnetic convective and slip flow due to a rotating disk in the presence of viscous dissipation and Ohmic heating. Shateyi [6] investigated thermal radiation and buoyancy effects on heat and mass transfer over a semi-infinite stretching surface with suction and blowing.

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In recent years, progress has been considerably made in the study of heat and mass transfer in MHD flows due to its application in many devices, like the MHD power generators and Hall accelerators. Magnetohydrodynamic free convection finds applications in fluid engineering problems such as MHD pumps, accelerators and flow meters, plasma studies, nuclear reactors, geothermal energy extraction, *etc.* Srinivasa Raju *et.al* [7] discussed the Analytical and Numerical study of unsteady MHD free convection flow over an exponentially moving vertical plate with Heat Absorption. Pal and Talukdar [8] analyzed the combined effect of mixed convection with thermal radiation and chemical reaction on MHD flow of viscous and electrically conducting fluid past a vertical permeable surface embedded in a porous medium is analyzed.

The objective of the present paper is to study the thermal diffusion and chemical reaction effects on unsteady magneto hydro dynamic flow of stratified viscous fluid.

Formulation of the problem

The study of Heat and Mass Transfer Thermal Diffusion Effect on MHD Free Convection Flow of Stratified Viscous Fluid with assumptions of temperature of plate is constant. Viscous and Darcy's resistance terms are taken into account with constant permeability of the medium. The suction velocity normal to the plate is constant.

$$(V' = -u_0) \text{ (Boussinesq approximation is valid)}$$

We considered a system of rectangular co-ordinates $O(x', y', z')$ where as $y' = 0$ on the plate and leading edge is z' axis. The density variation with temperature is considered while of all fluid properties remain constant. Due to the influence of density variation in the terms of the momentum and the energy equation and the variation of the expansion coefficient with temperature is neglected.

Continuity equation:

$$\frac{\partial V'}{\partial y'} = 0 \quad (1)$$

Momentum equation:

$$\frac{\partial u'}{\partial t'} + V' \frac{\partial u'}{\partial y'} = \nu \frac{\partial^2 u'}{\partial y'^2} + g\beta(T' - T_\infty^1) + g\beta^*(C' - C_\infty) - \left(\frac{\sigma B_0^2}{\rho(1+m^2)} + \frac{\nu}{K'} \right) u' \quad (2)$$

Energy Equation:

$$\frac{\partial T'}{\partial t'} + V' \frac{\partial T'}{\partial y'} = \frac{k\nu}{\mu c_p} \frac{\partial^2 T'}{\partial y'^2} \quad (3)$$

Diffusion equation:

$$\frac{\partial C'}{\partial t'} + V' \frac{\partial C'}{\partial y'} = D \frac{\partial^2 C'}{\partial y'^2} + D_1 \frac{\partial^2 C'}{\partial y'^2} - Kr^*(C' - C_\infty) \quad (4)$$

Where C_p -specific heat at constant pressure, g -Gravity due to Acceleration, k -Thermal conductivity, T' -Temperature of the fluid at the plate, T_∞^1 -temperature of the fluid at infinity, m is the hall current parameter.

u', v' are the Velocity components, ρ - Density of the fluid, ν -Kinematic viscosity, β and β^* -the thermal and concentration expansion coefficient respectively, B_0 -magnetic induction, D is the concentration diffusivity, K' -the permeability of the porous medium, C' -is the dimensional concentration, C_∞ -is the concentration of free stream, μ -coefficient of viscosity, D_1 -the thermal diffusivity. Kr^* -chemical reaction factor and m is the hall current parameter.

The boundary conditions for the velocity, temperature and concentration fields are:

$$\begin{aligned} u' = 0, T' = T_w', C' = C_w' \text{ at } y' = 0 \\ u' \rightarrow 0, T' \rightarrow T_\infty', C' \rightarrow C_\infty \text{ as } y' \rightarrow \infty \end{aligned} \quad (5)$$

Where T_w' and C_w' are the wall dimensional temperature and concentration respectively.

In order to write the governing equations and boundary condition in dimension less form the following non dimensional quantities are introduced.

$$u = \frac{u'}{u_o}, V = \frac{V'}{u_o}, t = \frac{t'u_o^2}{\nu}, y = \frac{y'u_o}{\nu}, \theta = \frac{T' - T_\infty'}{T_w' - T_\infty'}, C = \frac{C' - C_\infty'}{C_w' - C_\infty'}, Gr = \frac{\nu g \beta (T_w' - T_\infty')}{u_o^3}, K = \frac{u_o^2 K'}{\nu^2}, Pr = \frac{\mu C_p}{k},$$

$$M = \frac{\sigma B_o^2 \nu}{\rho(1+m^2)u_o^2}, Sc = \frac{\nu}{D}, Kr = \frac{K_r^* \nu}{u_o^2}, A = \frac{D_1(T_w' - T_\infty')}{(C_w' - C_\infty')\nu}, N_o = \frac{\beta^*(C_w' - C_\infty')}{\beta(T_w' - T_\infty')} \quad (6)$$

where Pr is the Prandtl number, Gr is the Grashof number, N_o is the buoyancy ratio, Sc is the Schmidt number, M is the magnetic parameter, K is the permeability parameter, A is the Thermal Diffusion parameter, Kr is the chemical reaction parameter.

In view of (6), the equations (2), (3), (4) reduced to the following dimensionless form

$$\frac{\partial u}{\partial t} - \frac{\partial u}{\partial y} = Gr\theta + N_o C + \frac{\partial^2 u}{\partial y^2} - \left(M + \frac{1}{K}\right)u, \quad (7)$$

$$\frac{\partial \theta}{\partial t} - \frac{\partial \theta}{\partial y} = \frac{1}{Pr} \frac{\partial^2 \theta}{\partial y^2} \quad (8)$$

$$\frac{\partial C}{\partial t} - \frac{\partial C}{\partial y} = \frac{1}{Sc} \frac{\partial^2 C}{\partial y^2} - KrC + A \frac{\partial^2 \theta}{\partial y^2} \quad (9)$$

And these corresponding boundary conditions are

$$t > 0: u=0, \theta=1, C=1 \text{ at } y=0, \quad u \rightarrow 0, T \rightarrow 0, C \rightarrow 0 \text{ as } y \rightarrow \infty \quad (10)$$

NUMERICAL SOLUTION USING FINITE ELEMENT METHOD

Finite element technique is used to solving the non-dimensional momentum and energy equations (7) (8) and (9) along with the imposed boundary conditions (10).

The Galerkin expression for the differential equation (7) becomes

$$\int_{y_j}^{y_k} \left\{ N^T \left[\frac{\partial^2 u^{(e)}}{\partial y^2} - \frac{\partial u^{(e)}}{\partial t} + \frac{\partial u^{(e)}}{\partial y} - Ru^{(e)} + P \right] \right\} dy = 0$$

$$\text{Where } N^T = [N_j \quad N_k]^T = \begin{bmatrix} N_j \\ N_k \end{bmatrix}, R = M + \frac{1}{K}, P = (G_r)T + (G_r)N_o C;$$

Let the linear piecewise approximation solution

$$u^{(e)} = N_j(y)u_j(t) + N_k(y)u_k(t) = N_j u_j + N_k u_k$$

The element equation is given by

$$\int_{y_j}^{y_k} \left\{ \begin{bmatrix} N_j' & N_j' \\ N_j' & N_k' \end{bmatrix} \begin{bmatrix} u_j \\ u_k \end{bmatrix} \right\} dy + \int_{y_j}^{y_k} \left\{ \begin{bmatrix} N_j & N_j & N_j & N_k \\ N_j & N_k & N_k & N_k \end{bmatrix} \begin{bmatrix} \dot{u}_j \\ \dot{u}_k \end{bmatrix} \right\} dy - \int_{y_j}^{y_k} \left\{ \begin{bmatrix} N_j & N_j' & N_j & N_k' \\ N_j' & N_k & N_k' & N_k \end{bmatrix} \begin{bmatrix} u_j \\ u_k \end{bmatrix} \right\} dy$$

$$+ R \int_{y_j}^{y_k} \left\{ \begin{bmatrix} N_j & N_j & N_j & N_k \\ N_j & N_k & N_k & N_k \end{bmatrix} \begin{bmatrix} u_j \\ u_k \end{bmatrix} \right\} dy = P \int_{y_j}^{y_k} \begin{bmatrix} N_j \\ N_k \end{bmatrix} dy$$

Where prime and dot denotes differentiation w.r.t. 'y' and 't' respectively Simplifying we get

$$\frac{1}{l^{(e)2}} \begin{bmatrix} 1 & -1 \\ -1 & 1 \end{bmatrix} \begin{bmatrix} u_j \\ u_k \end{bmatrix} + \frac{1}{6} \begin{bmatrix} 2 & 1 \\ 1 & 2 \end{bmatrix} \begin{bmatrix} \dot{u}_j \\ \dot{u}_k \end{bmatrix} - \frac{1}{2l^{(e)}} \begin{bmatrix} -1 & 1 \\ -1 & 1 \end{bmatrix} \begin{bmatrix} u_j \\ u_k \end{bmatrix} + \frac{R}{6} \begin{bmatrix} 2 & 1 \\ 1 & 2 \end{bmatrix} \begin{bmatrix} u_j \\ u_k \end{bmatrix} = \frac{P}{2} \begin{bmatrix} 1 \\ 1 \end{bmatrix}$$

$$\text{where } l^{(e)} = y_k - y_j = h$$

In order to get the differential equation at the knot x_i , we write the element equations for the elements $y_{i-1} \leq y \leq y_i$ and $y_i \leq y \leq y_{i+1}$ assemble two element equations, we obtain

$$\frac{1}{l^{(e)2}} \begin{bmatrix} 1 & -1 & 0 \\ -1 & 2 & -1 \\ 0 & -1 & 1 \end{bmatrix} \begin{bmatrix} u_{i-1} \\ u_i \\ u_{i+1} \end{bmatrix} + \frac{1}{6} \begin{bmatrix} \bullet \\ 2 & 1 & 0 \\ 1 & 4 & 1 \\ 0 & 1 & 2 \\ \bullet \\ u_{i-1} \\ u_i \\ u_{i+1} \end{bmatrix} - \frac{(1)}{2l^{(e)}} \begin{bmatrix} -1 & 1 & 0 \\ -1 & 0 & 1 \\ 0 & -1 & 1 \end{bmatrix} \begin{bmatrix} u_{i-1} \\ u_i \\ u_{i+1} \end{bmatrix} + \frac{R}{6} \begin{bmatrix} 2 & 1 & 0 \\ 1 & 4 & 1 \\ 0 & 1 & 2 \end{bmatrix} \begin{bmatrix} u_{i-1} \\ u_i \\ u_{i+1} \end{bmatrix} = \frac{P}{2} \begin{bmatrix} 1 \\ 2 \\ 1 \end{bmatrix}$$

We put the row equation corresponding to the knot 'i', is

$$\frac{1}{l^{(e)2}} [-u_{i-1} + 2u_i - u_{i+1}] + \frac{1}{6} \begin{bmatrix} \bullet \\ u_{i-1} + 4u_i + u_{i+1} \\ \bullet \\ \bullet \end{bmatrix} - \frac{(1)}{2l^{(e)}} [-u_{i-1} + u_{i+1}] + \frac{R}{6} [u_{i-1} + 4u_i + u_{i+1}] = P$$

Applying Crank-Nicholson method to the above equation then we get

$$A_1 u_{i-1}^{n+1} + A_2 u_i^{n+1} + A_3 u_{i+1}^{n+1} = A_4 u_{i-1}^n + A_5 u_i^n + A_6 u_{i+1}^n + 24Pk$$

Where $A_1 = 2 + (3*r*h) + (R*k) - (6*r)$; $A_2 = (4*R*k) + (12*r) + 8$; $A_3 = 2 + (R*k) - (6r) - (3*h*r)$;
 $A_4 = 2 - (R*k) - (3*r*h) + (6*r)$; $A_5 = 8 - (4*R*k) - (12*r)$; $A_6 = 2 - (R*k) + (3*r*h) + (6*r)$; (11)
 $P = (G_r)T_i^j + (G_r)N_o C_i^j$;

Applying similar procedure to equation (8), we get

$$B_1 T_{i-1}^{n+1} + B_2 T_i^{n+1} + B_3 T_{i+1}^{n+1} = B_4 T_{i-1}^n + B_5 T_i^n + B_6 T_{i+1}^n \quad (12)$$

$$B_1 = (2*Pr) + (3*(Pr)*r*h) - (6*r); B_2 = (8*Pr) + (12*r); B_3 = (2*Pr) - (3*(Pr)*r*h) - (6*r);$$

$$B_4 = (2*Pr) - (3*(Pr)*r*h) + (6*r); B_5 = (8*Pr) - (12*r); B_6 = (2*Pr) + (3*(Pr)*r*h) + (6*r);$$

Applying similar procedure to equation (9), we get

$$J_1 C_{i-1}^{n+1} + J_2 C_i^{n+1} + J_3 C_{i+1}^{n+1} = J_4 C_{i-1}^n + J_5 C_i^n + J_6 C_{i+1}^n \quad (13)$$

$$J_1 = (2*Sc) + (3*Sc*r*h) - (6*r) + (Kr*Sc*k); J_2 = (8*Sc) + (12r) + (4*Kr*Sc*k); J_3 = (2*Sc) - (3*Sc*r*h) - (6*r) + (Kr*Sc*k);$$

$$J_4 = (2*Sc) - (3*Sc*r*h) + (6*r) - (Kr*Sc*k); J_5 = (8*Sc) - (12r) - (4*Kr*Sc*k); J_6 = (2*Sc) + (3*Sc*r*h) + (6*r) - (Kr*Sc*k);$$

Where Here $r = \frac{k}{h^2}$ and k, h are mesh sizes along y- direction and time-direction respectively index 'i' refers to space and 'j' refers to time .The mesh system consists of h=0.1 and k=0.001.

In the equations (11), (12), and (13), taking $i = 1(1) n$ and using boundary conditions (10), then we get the following system of equations are obtained:

$$A_i X_i = B_i \text{ for } i=1(1)n$$

Where A_i 's are matrices of order n and X_i , B_i 's are column matrices having n-components. The solutions of above system of equations are obtained by using Thomas Algorithm for velocity, temperature and concentration. Also, numerical solutions for these equations are obtained by C++ program. In order to prove the convergence and stability of Galerkin finite element method, the same C++ program was run with smaller values of h and k, no significant change was observed in the values of u, T and C. Hence the Galerkin finite element method is stable and convergent.

RESULTS AND DISCUSSION

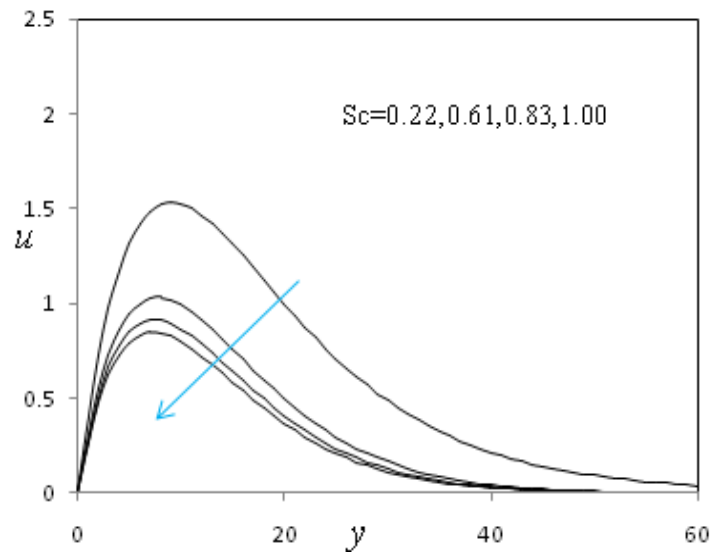


Figure 1: Velocity Profiles for different values of Sc when $Gr=2$, $K=100$, $M=0.02$, $Pr=0.71$, $Kr=1.0$, $A=0.2$, $No=1.5$.

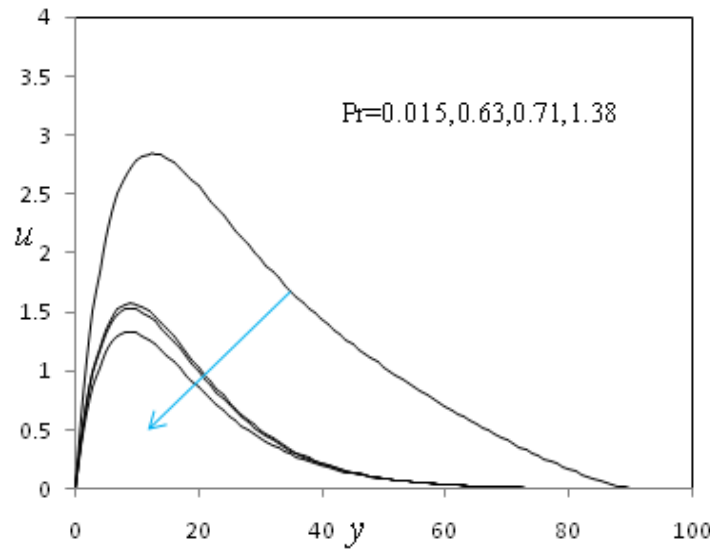


Figure 2: Velocity Profiles for different values of Pr when $Gr=2$, $K=100$, $M=0.02$, $Sc=0.22$, $Kr=1.0$, $A=0.2$, $No=1.5$.

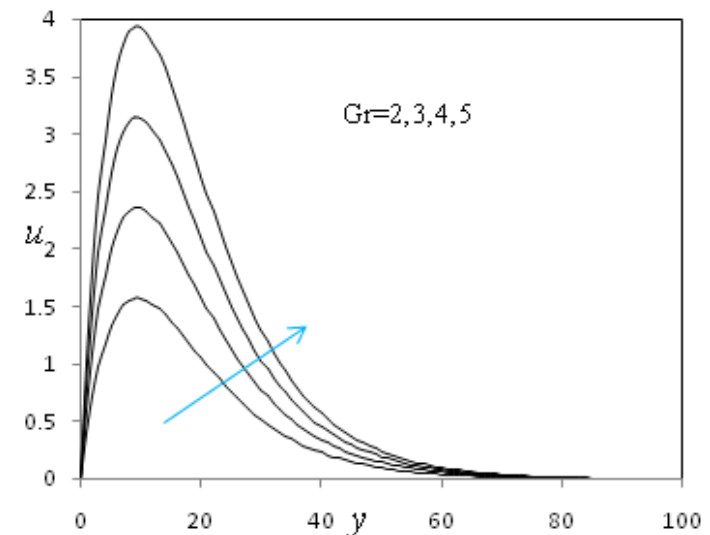


Figure 3: Velocity Profiles for different values of Gr when $Pr=0.71$, $K=100$, $M=0.02$, $Sc=0.22$, $Kr=1.0$, $A=0.2$, $No=1.5$

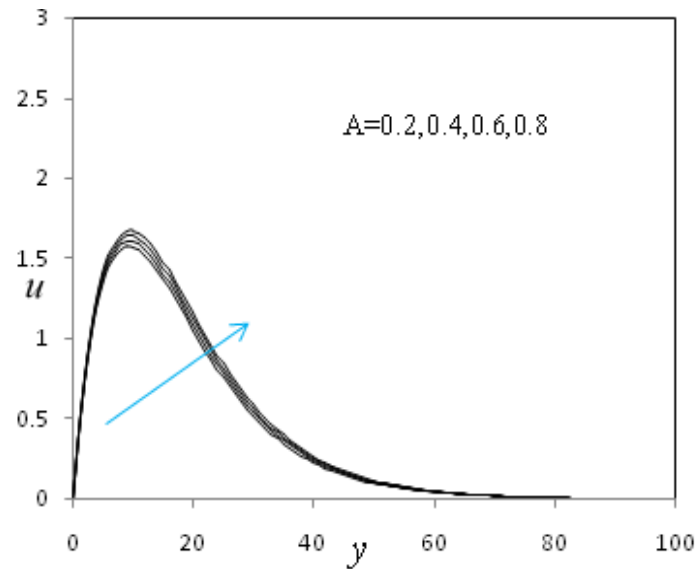


Figure 4: Velocity Profiles for different values of A when $Pr=0.71$, $K=100$, $M=0.02$, $Sc=0.22$, $Kr=1.0$, $Gr=0.2$ $No=1.5$

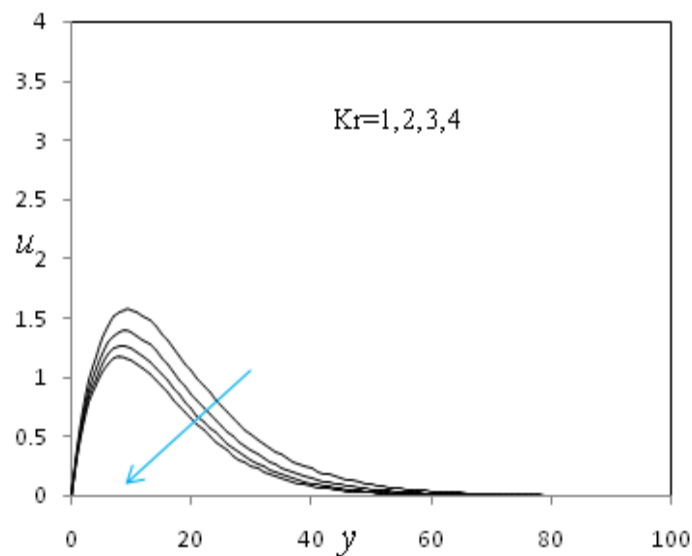


Figure 5: Velocity Profiles for different values of Kr when $Pr=0.71$, $K=100$, $M=0.02$, $Sc=0.22$, $A=0.2$, $No=1.5$

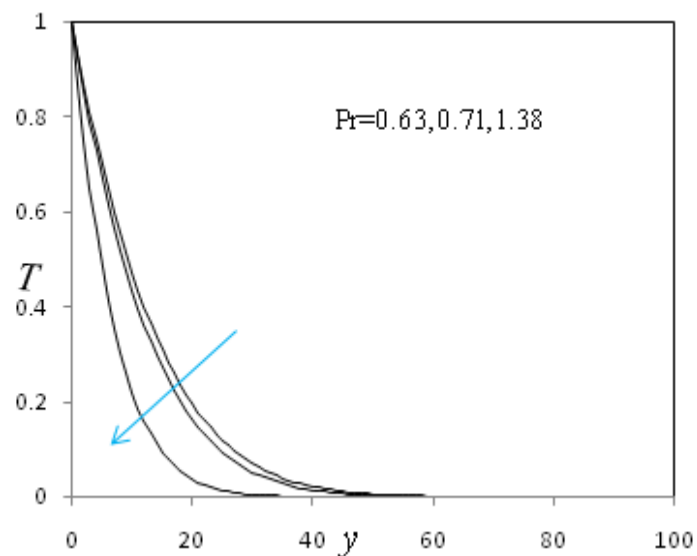


Figure 6: Temperature Profiles for different values of Pr when $Gr=2.0$, $K=100$, $M=0.02$, $Sc=0.22$, $Kr=1.0$, $A=0.2$, $No=1.5$

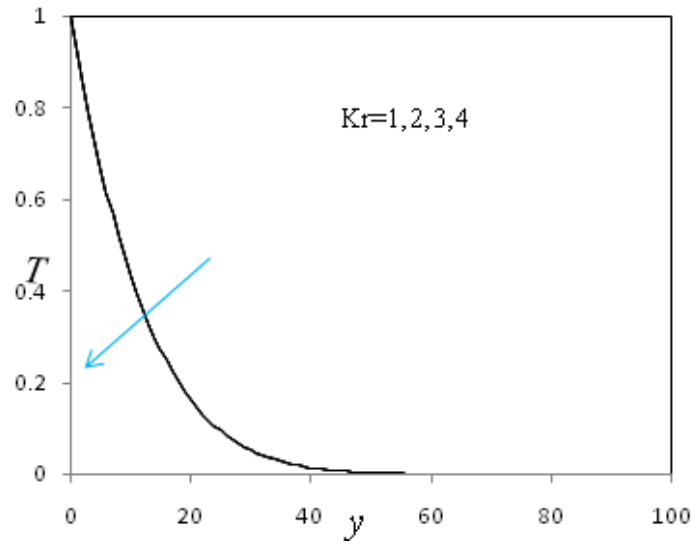


Figure 7: Temperature Profiles for different values of Kr when $Gr=2.0$, $K=100$, $M=0.02$, $Sc=0.22$, $Pr=0.71$, $A=0.2$, $No=1.5$

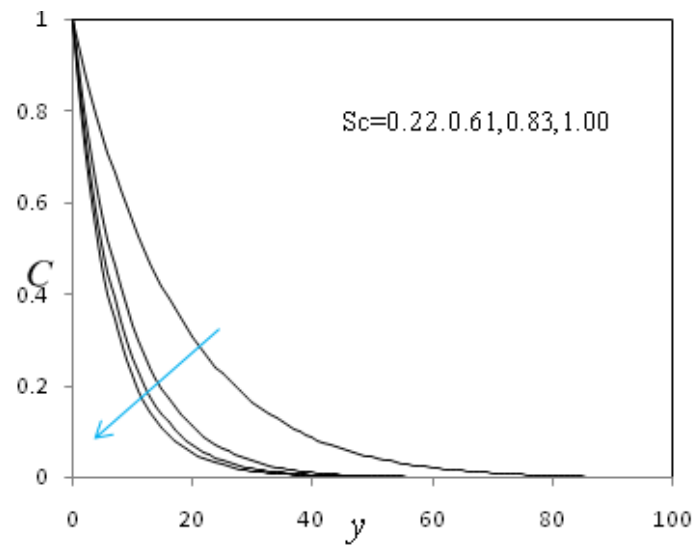


Figure 8: Concentration Profiles for different values of Sc when $Gr=2.0$, $K=100$, $M=0.02$, $Kr=1.0$, $A=0.2$, $No=1.5$

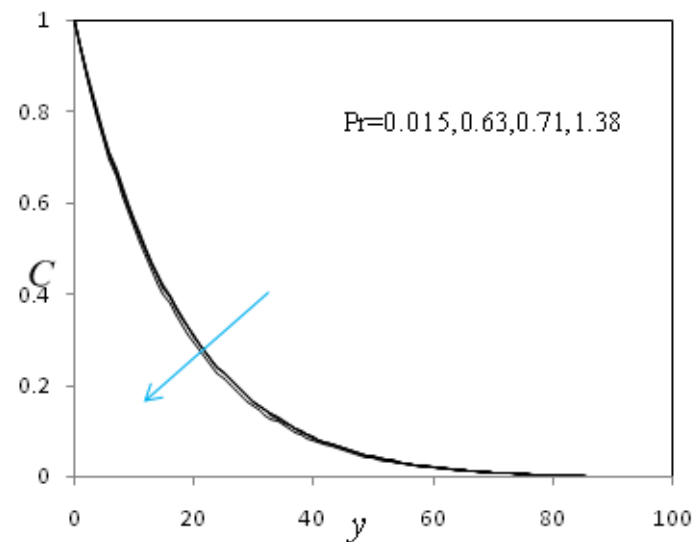


Figure 9: Concentration Profiles for different values of Pr when $Gr=2.0$, $Sc=0.22$, $K=100$, $M=0.02$, $Kr=1.0$, $A=0.2$, $No=1.5$

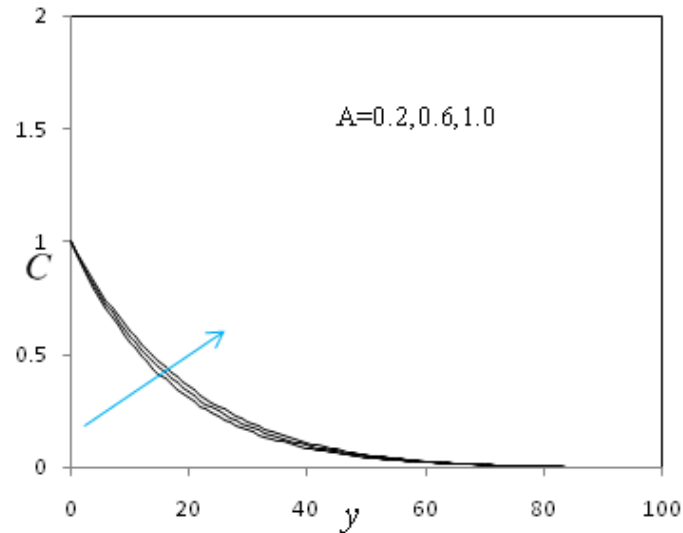


Figure 10: Velocity Profiles for different values of A when $Pr=0.71$, $K=100$, $M=0.02$, $Sc=0.22$, $Kr=1.0$, $Gr=0.2$ $No=1.5$

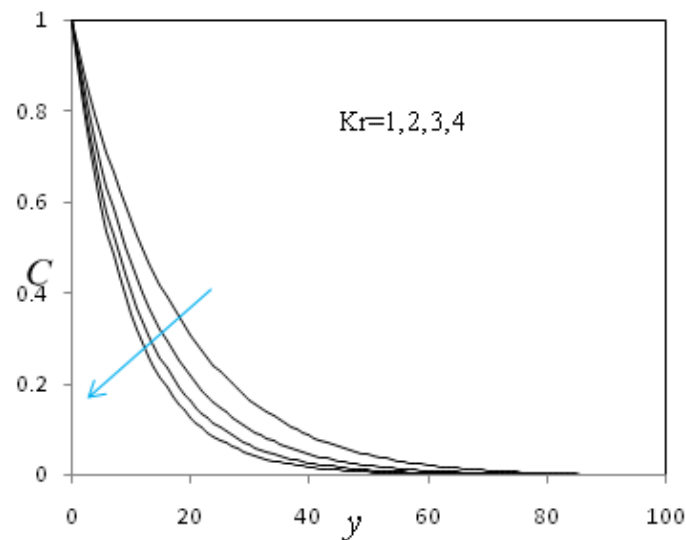


Figure 11: Concentration Profiles for different values of Kr when $Gr=2.0$, $Sc=0.22$, $K=100$, $M=0.02$, $Pr=0.71$ $A=0.2$, $No=1.5$.

Velocity distribution of fluid flow is plotted from Figure 1 to 5.

From Figure 1 It is clearly observed that Velocity decreases with an increase of Schmidt number. The following values of Schmidt number $Sc=0.22$ (Helium), 0.66 (Ammonia and Water Vapour), 0.83 (oxygen), 1 (carbon dioxide) are considered to plot the Figure 1.

The velocity profile for different values of Prandtl number (Mercury (0.015), oxygen (0.63), Air (0.71, ammonia (1.38)) is plotted in Figure 2 and it is found that velocity decreases with an increase of Prandtl number.

From the Figures 3 to 5 It is also observed that velocity increases with the increase in Gr, & Thermal diffusion parameter A, velocity decreases with an increase in chemical reaction parameter Kr.

Temperature distribution of fluid flow is plotted in Figure 6 and 7. we observed that the temperature does not fluctuate with change in Gr(Grashof number) and A (Thermal Diffusion parameter) and Sc(Schmidt number). Temperature decreases with an increase in Prandtl number (Pr) and Chemical Reaction parameter (Kr).

Concentration distribution of fluid flow is plotted from Figure 8 to 11. from the figures 8,9 and 11 concentration profile decreases with an increase in Sc, Pr, and Kr, concentration increases with an increase in A which is observed in figure 10.

CONCLUSION

In this paper we have studied the Thermal diffusion and chemical reaction effects on MHD Free convective flow of stratified viscous fluid with heat and mass transfer. From present numerical study the following conclusions can be drawn

- 1) The velocity increases with the increase of Gr.
- 2) The velocity and concentration decreases with an increase in Schmidt number.
- 3) The velocity and concentration increases with an increase in the thermal diffusion parameter.
- 4) Increasing the prandtl number substantially decreases the velocity and the temperature profiles.
- 5) The velocity as well as concentration decreases with an increase in the chemical reaction parameter.

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